



# Comparing Effects of Feedstock and Run Conditions on Fast Pyrolysis Products Produced at the Pilot Scale: Solids Management from an Operational Perspective

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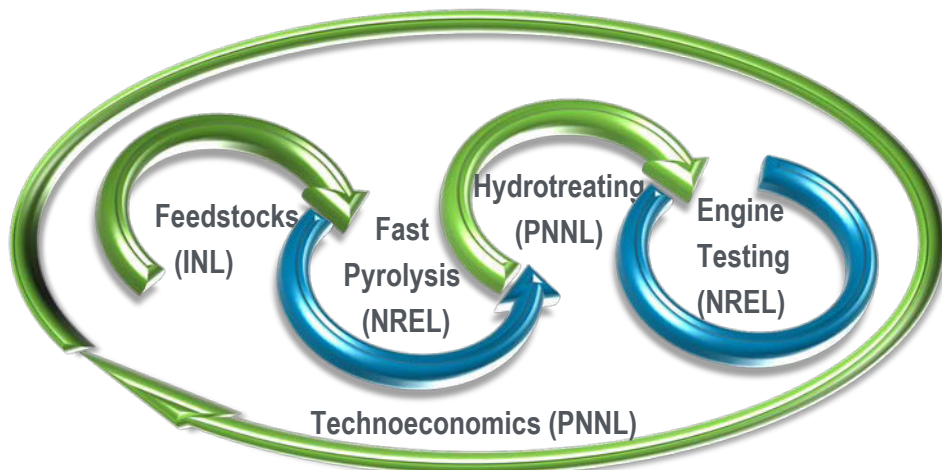
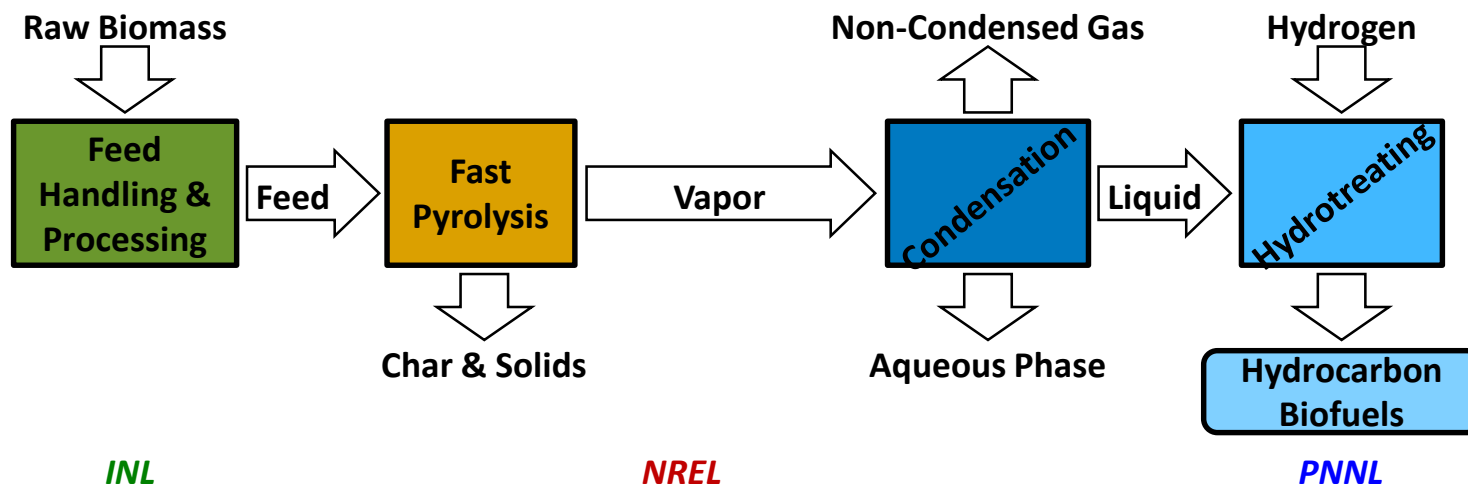
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# “Field to Fleet” Fast Pyrolysis Verification

**Objective: Conduct preliminary pilot-scale tests to down select feedstock and operating conditions for the verification run.**



## BETO FY17 Performance Goal:

*“Validate at a pilot scale at least one technology pathway for hydrocarbon biofuel production at a mature modeled price of \$3/GGE with GHG emissions reduction of 50% or more compared to petroleum fuel.”*

-BETO MYPP 2016

# TCPDU Flow Diagram – Configured for Fast Pyrolysis

½ Ton/Day

Continuous feed plant

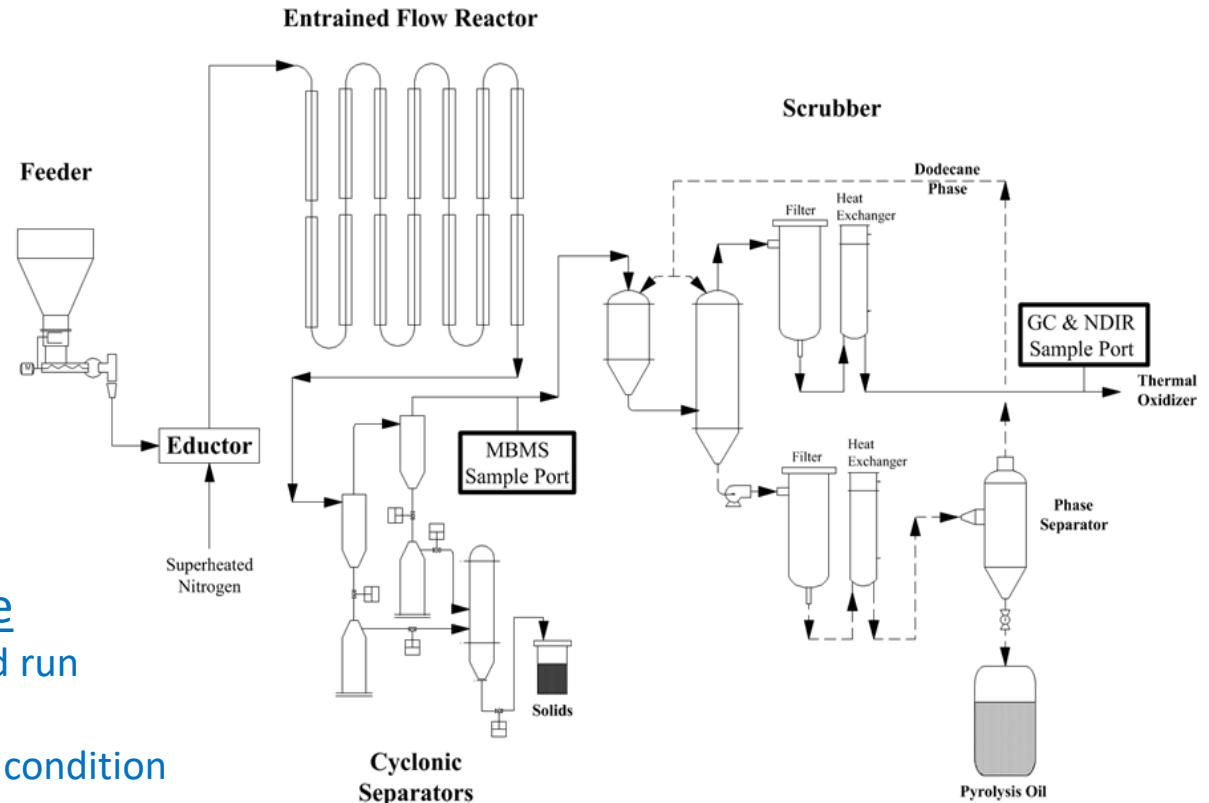
Variable Residence Time

Variable Temperature

Variable Flowrate

## Sample Procedure

- Pyrolyse feedstock at determined run conditions and steady state
- Collect 5 gallon sample of oil per condition
- Collect char throughout run
- Analyze light gasses and pyrolysis vapors during run
- Residual carbon oxidation ‘burnout’ performed between trials
- Quenching fluid changed between feedstocks



Fast Pyrolysis: Thermochemical decomposition of biomass in the absence of oxygen at elevated temperatures

# Blended feedstocks tested for demonstration

- Delivered cost target <\$90/dry ton (biomass)
- Conversion target ~\$2.53/GGE (2014\$)
- Industrially relevant

## Benefits of Blends:

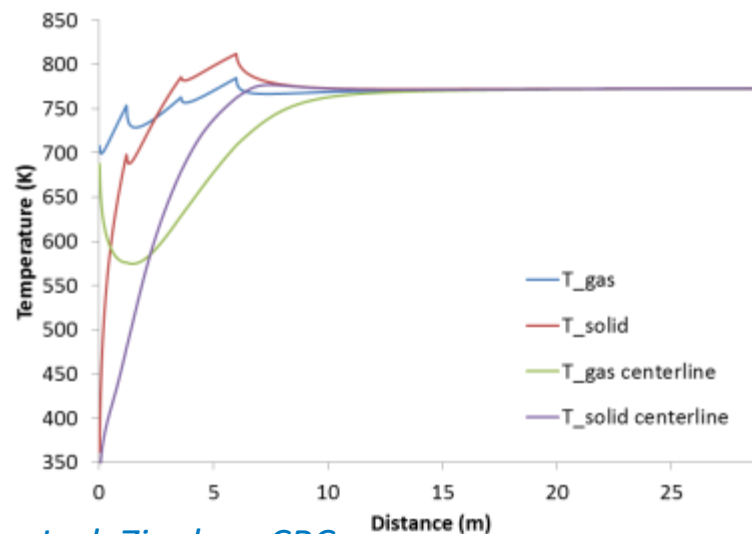
- Increase resources available
- Dilution of negative characteristics
- Enhancement of positive characteristics
- Lower feedstock cost

Feedstock	Oak	Clean Pine	CP <sub>30</sub> FR <sub>35</sub> C&D <sub>25</sub> SW <sub>10</sub>	CP <sub>45</sub> FR <sub>25</sub> C&D <sub>30</sub>
Est. Feedstock Cost (\$/dry ton)	>\$100.00	\$99.50	\$75.10	\$79.10
Other Notes	Baseline material used by TCPDU	Baseline material used by INL & PNNL.	PNNL design case blend	All-woody version of blend

CP = Clean Pine, FR = Forestry Residues, C&D = Construction and Demolition waste, SW = Switchgrass

# Initial Operating Conditions Chosen Based on Modeling

Condition	1	2	3
Reactor Temp	500°C	500°C	480°C
# of reactor zones	12	4	4
Residence Time	~ 3.5 sec	~ 0.9 sec	~ 0.9 sec
Other Notes	Standard TCPDU operating condition	Slightly over time required for particle to get to temp based on model	Reaction temp oils PNNL uses



Jack Ziegler - CPC

Modeling & operational data show that solids in the entrained flow reactor reach temperature in less than 3 zones.



# Initial Run Conditions Not Viable

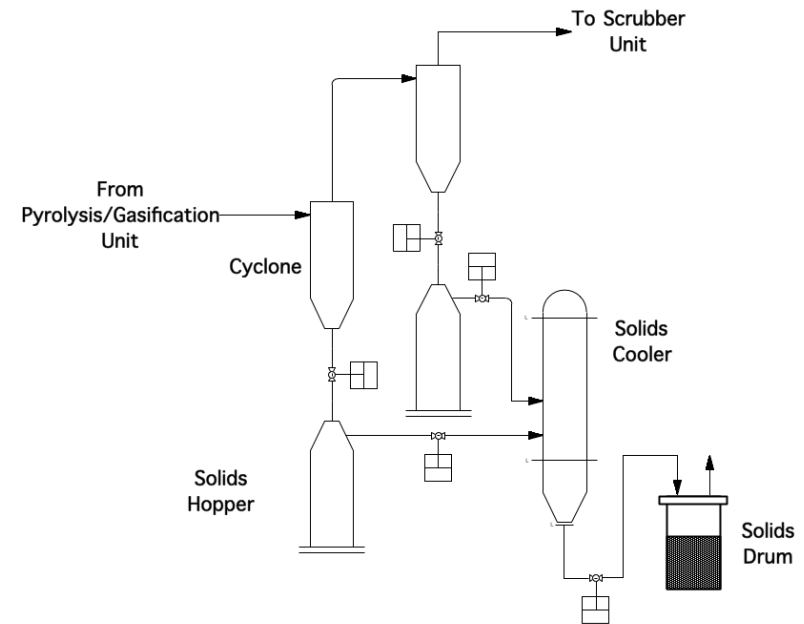


- Plant shut downs necessary within 15 minutes of starting feed due to char plugging cyclones or continuing to condensation chain
- Unable to run consistently enough to perform 5 gallon runs

# Char collection problems presented in two ways

- Char not flowing through collection system
  - Required immediate on the fly plant maintenance
  - Resulted in loss of char
- Sending char to the scrubber
  - Requires shut down of feed for significant plant maintenance
  - Resulted in loss of char and oil used in mass balance

## TCPDU Cyclonic Separator System



Further characterization required!





# Additional Experiments Performed to Characterize Problems

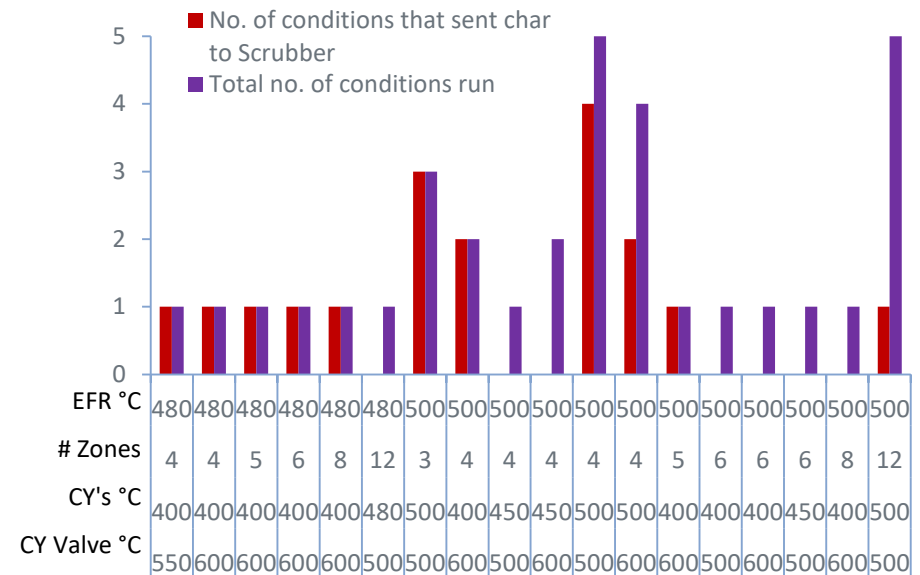
## Hypotheses

- Sticky char caused by under-cracking (Under-pyrolyzing)
- Sticky char caused by over-cracking (Polymerizing)
- Non-ideal char particle size distribution (PSD)
- Cyclone build-up/obstruction

## Lessons Learned

- Short residence times/less severe pyrolysis led to char in scrubber
- Longer residence times/more severe pyrolysis decreased operational difficulties

## Trials conducted with Pine Feedstock to characterize char collection problems





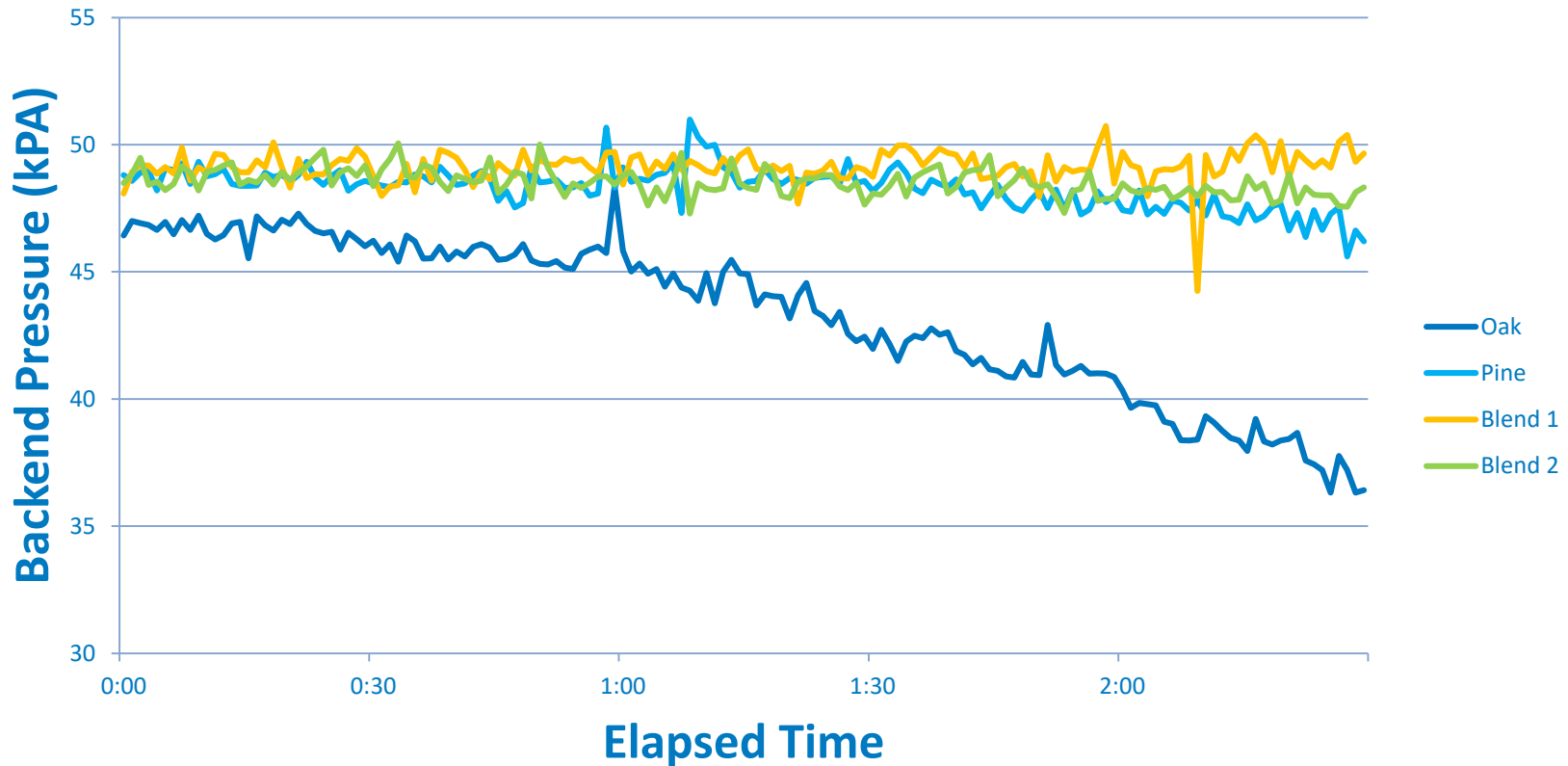
# New operating conditions chosen

Condition	1	2	3
Reactor Temp	500°C	500°C	480°C
# of reactor zones	12	9	12
Residence Time	~ 3.5 sec	~ 2.6 sec	~ 3.5 sec
Other Notes	Standard TCPDU operating condition	Slightly over time required for particle to get to temp based on model	Reaction temp oils PNNL uses

- Less severe conditions lead to increased operational problems
- Smaller native particle size of oak feed presumed to aid in plant operations

# Pressure effects observed running different feedstocks

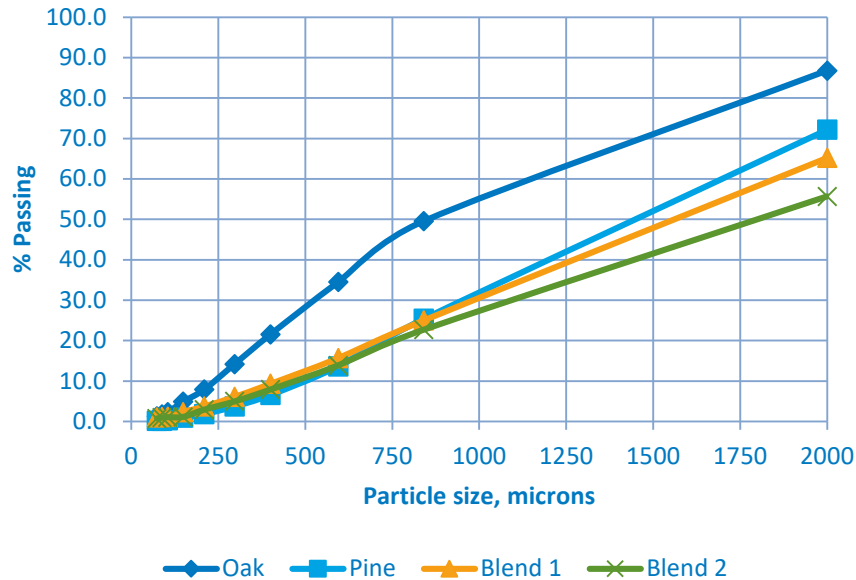
Back-end TCPDU at 500°C, ~2.9 sec



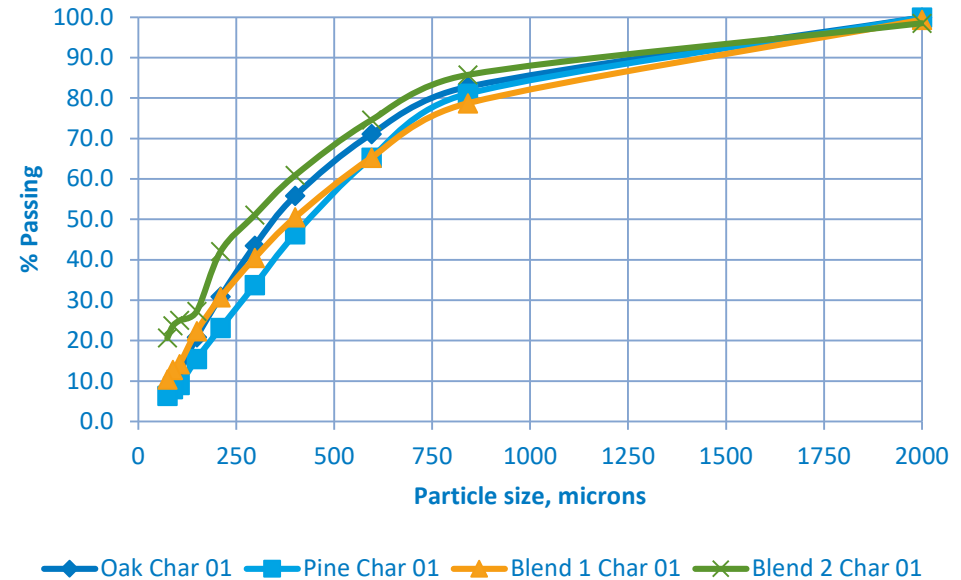
- Pressure drop due to build up of carbon/oil deposits at condensation chain inlet

# Feedstock particle size relation to system pressure drop

## Crushed Feed



## Collected Char



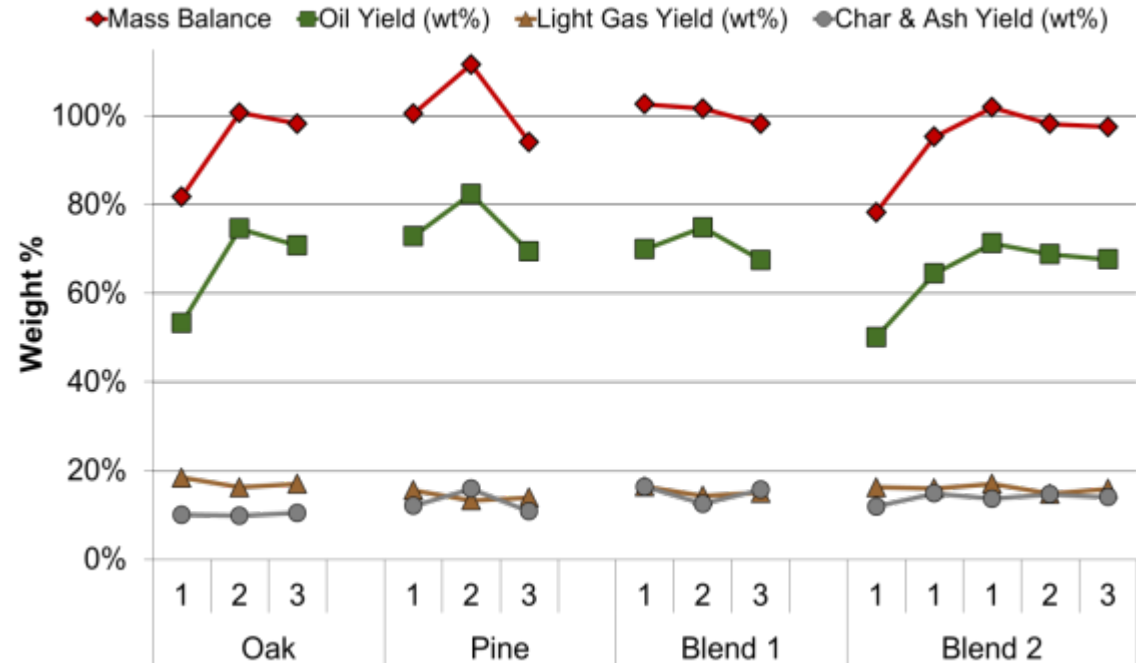
- Crushed Oak feed contained larger distribution of smaller particles
- Collected char samples contained similar size distribution regardless of feedstock
- Small particles in oak feed thought to volatilize more completely, though fine solids likely carried through cyclones and into condensation chain inlet, causing system pressure drop
- Oak pellets made from sawdust, where pine pellets made from native wood milled to ~2mm.
- Pellets very similar in size

# Mass Balances Difficult to Obtain with Short run times

## Lesson Learned:

- Mass lost due to char plugging complicates mass balance
- TCPDU optimized for larger runs-5 gallon runs at operational fringe for data resolution
- Scrubber requires ~8 hours to equilibrate in order to achieve consistent oil yields

## Mass Balance & Product Yield Results



- Replicates of Blend 2, condition 1 run to verify reproducibility of results
- Trials run 12131

System brought to steady state operation conditions prior to collection of 5 gallon samples

# Conclusions

- Essential to run tests prior to large demonstrations
- Optimum operating conditions depend on feedstock
- Under pyrolyzed material difficult to manage operationally
- Solids management is difficult but very important
- Pilot scale demonstration is critical to verify chemistry and operational scalability

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**DOE BETO**



# Thank you!

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