



Conversion, stability, and selectivity improvements through catalyst development for the reductive etherification reaction

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better fuels | better vehicles | sooner

**ENERGY** Energy Efficiency & Renewable Energy

# Waste-to-biofuel upgrading





Goal of upgrading low or negative cost feedstocks into targeted bioblendstocks

# Ether production process





### Iteration on technoeconomic analysis (TEA):

- Major TEA cost drivers include conversion, space velocity, selectivity-specifically dibutyl ether (DBE)
- Assumptions on catalyst stability and regenerability



ΔMFSP (\$/GGE) Current Case \$2.94

Tornado plot showing impact of various sensitivities on MFSP for the "Current Case."



Cost comparison for DBE-Free (neglecting dibutyl ether formation) and Best Case (100% selectivity to the target) scenarios relative to the experimentally based Current Case analysis.

#### Collaboration with TEA shows cost drivers and critical assumptions

# **Reductive etherification**





Dual Catalyst System:

- Pd expected to be fairly stable
- Solid acids are known to absorb water and deactivate
- Side reactions on acidic surfaces can form inhibitory coking

**Continuous flow reaction:** 



Continuous flow test: 0.25 mL/min of equimolar 4heptanone & n-butanol, 2.2 g Pd/C, 6.6 g A-15, 120  $^{\circ}$ C, 1000 psig H<sub>2</sub> (3-4 fold excess)

### Continuous flow reaction seems to show catalyst deactivation

### Solid acid deactivation

![](_page_4_Picture_1.jpeg)

### Carbon deposition:

![](_page_4_Figure_3.jpeg)

Decrease in reaction rate of dimethylether over zeolite-based catalysts ACS Catalysis 2015, 5, 1794-1803

Water adsorption:

 $H_2O$ 

H<sub>2</sub>O

H<sub>2</sub>O

H<sub>2</sub>O

 $H_2O$ 

![](_page_4_Figure_6.jpeg)

Comparison of initial etherification rate and water concentration over Amberlyst-70 Chemical Engineering Journal 2014, 246, 71–78

Deactivation can occur through carbon deposition or water adsorption

### Tailored solid acids

![](_page_5_Picture_1.jpeg)

![](_page_5_Figure_2.jpeg)

ACS Catal., 2018, 8 (1), pp 372-391

### **Overall goal:**

- Improved aqueous stability
- Improved thermal stability
- High acid site density
- Low cost materials

#### Phosphated metal oxides:

- Reported to be water-tolerant
- Thermally stable
- Varied acidities and material costs

![](_page_5_Figure_13.jpeg)

Metal oxide surface modification with phosphoric acid

Water-tolerant acids could lead to increased stability and facile regenerability

# Acidity characterization

![](_page_6_Picture_1.jpeg)

![](_page_6_Figure_2.jpeg)

 $NH_3$ -TPD results for total acidity measurements (Amberlyst-15 reported to be 4600  $\mu$ mol/g)

![](_page_6_Figure_4.jpeg)

Pyridine-DRIFTS spectra showing the relative amounts of Brønsted and Lewis acid sites.

### Phosphating procedure increases Brønsted/Lewis ratio and possibly total acidity

# Hydrophobicity evaluation

![](_page_7_Figure_1.jpeg)

![](_page_7_Figure_2.jpeg)

Thermogravimetric analysis of catalysts after treatment in saturated water chamber for 72 h.

Little effect on acidity vs. hydrophobicity but reported to maintain catalytic efficiency

### Acidity and water adsorption results show little change in hydrophobicity

### Metal oxide batch testing

![](_page_8_Picture_1.jpeg)

![](_page_8_Picture_2.jpeg)

High-pressure batch reactors

![](_page_8_Picture_4.jpeg)

![](_page_8_Figure_5.jpeg)

20 mL equimolar 4-heptanone & n-butanol, 231 mg Pd/Carbon, 681 mg solid acid, 120 or 190 °C, 1000 psig H<sub>2</sub>,1 h.

Increasing temperature improves ether yield and selectivity but A-15 is limited

### Flow reaction tests

![](_page_9_Picture_1.jpeg)

![](_page_9_Picture_2.jpeg)

C3PO: a high-pressure trickle bed flow reactor

![](_page_9_Figure_4.jpeg)

Significantly higher turnover (to acid sites) from metal oxide catalysts

Metal oxide stability was roughly double of the previous A-15 run

0.05 mL/min of equimolar 4-heptanone & n-butanol, 0.5 g Pd/C, 1.5 g acid catalyst, 1000 psig  $H_2$ 

![](_page_9_Figure_8.jpeg)

Increase in 4-BH Yield of 5%, increase in DBE yield of 7.5-fold

# Single-phase catalyst

![](_page_10_Picture_1.jpeg)

![](_page_10_Figure_2.jpeg)

20 mL equimolar 4-heptanone & n-butanol, 231 mg Pd/Carbon, 681 mg solid acid, 1000 psig  $H_2$ , 1 h.

Pd crystallite size from X-Ray Diffraction spectroscopy using FWHM of 40° Pd peak

### Single-phase catalysts show superior results in batch testing

# Reaction pathway

![](_page_11_Figure_1.jpeg)

![](_page_11_Figure_2.jpeg)

20 mL equimolar 4-heptanone (or 4-heptanol) & n-butanol, 231 mg Pd/Carbon, 681 mg solid acid, 1000 psig  $H_2$  (or He), 1 h.

Reaction seems to proceed through ketalization pathway of reductive etherification

# Reaction pathway

![](_page_12_Picture_1.jpeg)

### **Route A: Reduction, then etherification**

![](_page_12_Figure_3.jpeg)

### **Route B: Ketalization, then etherification**

![](_page_12_Figure_5.jpeg)

### Metal & Acid:

Applied Catalysis A: General **2000**, 191,153–162 Catalysts **2015**, 5 (4), 2244-2257 Green Chemistry **2018**, 20 (5), 1095-1105 Applied Catalysis B: Environmental **2019**, 258, 117793 Energy Technology **2019**, 7 (5), 1801071 Etc.

### Palladium & Acid:

Tetrahedron Letters, **1995**, 36 (24), pp. 4235-4236 Journal of Molecular Catalysis A: Chemical **2000**, 152 (1-2), 133-140. Bulletin of the Chemical Society of Japan **2005**, 78 (3), 456-463 Synlett **2006**, 20, 3489-3491. \*\*\*\*Green Chem., **2012**, 14, 1626 ACS Sustainable Chem. Eng. **2016**, 4, 4089–4093 ChemSusChem **2017**, 10, 2527 – 2533 Green Chemistry **2018**, 20 (9), 2110-2117 ChemSusChem **2018**, 11 (21), 3796-3802 RSC Advances **2019**, 9 (44), 25345-25350

Palladium is heavily favored for acetal/ketal pathway of ether formation

# Key takeaways

![](_page_13_Picture_1.jpeg)

### **Reductive etherification for targeted bioblendstocks**

![](_page_13_Figure_3.jpeg)

 Phosphated metal oxides show increased Bronsted acidity but similar hydrophobicity

![](_page_13_Figure_5.jpeg)

![](_page_13_Figure_6.jpeg)

 Nb<sub>2</sub>O<sub>5</sub>-PO<sub>4</sub> shows increased turnover and selectivity in flow reaction tests

![](_page_13_Figure_8.jpeg)

 Palladium-deposited onto TiO<sub>2</sub>-PO<sub>4</sub> at 7.5 wt% shows optimized yields enabling stronger regeneration conditions

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![](_page_14_Picture_1.jpeg)

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![](_page_14_Figure_11.jpeg)

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![](_page_15_Picture_0.jpeg)

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