

Pyrolysis Vapor and Bio-Oil Preconditioning via *Ex Situ* Hydrodeoxygenation and Alkylation Using a Heteropolyacid Catalyst

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Introduction

Ex situ catalytic preconditioning of biomass pyrolysis vapors (partial deoxygenation) has the potential for both reducing the oxygen content and beneficially influencing the oxygen speciation of condense bio-oils for enhancement of downstream condensed phase upgrading processes. Here, condensed phase upgrading processes may refer to both coprocessing and hydroprocessing with vacuum gas-oil (VGO). Reduction of oxygen content to produce bio-oils with greater hydrophobicity can enhance VGO-solubility while tailoring of oxygen speciation by removal of reactive carbonyls (e.g., acetic acid) can lessen catalytic deactivation via coking reactions.^{1,2} Furthermore, enhanced VGO-solubility and reduced coking leads to greater biogenic carbon incorporation in end-products from condensed phase upgrading processes. By leveraging the hydrodeoxygenation and alkylation activity of a titania-supported molybdenum-heteropolyacid ($\text{Mo-HPA}/\text{TiO}_2$) catalyst, pyrolysis vapors and resulting condensed bio-oils were effectively preconditioned for downstream upgrading.³ Data regarding the use of $\text{Mo-HPA}/\text{TiO}_2$ for pyrolysis vapor preconditioning will be presented on, including method of employment, catalyst characterization, and impacts on bio-oil in relation to downstream condensed phase upgrading processes. Our approach is to:

- Compare $\text{Mo-HPA}/\text{TiO}_2$ product distribution to HZSM-5.
- Investigate $\text{Mo-HPA}/\text{TiO}_2$ regeneration and characterize changes in acid site character.
- Assess product differences in terms of enhanced VGO-solubility.

Materials & Methods

- Used lab scale pulsed-flow catalyst screening equipment (Figure 1) to assess catalyst activity.
- Pyrolysis and upgrading conducted at 500°C and 400°C, respectively, using Loblolly pine biomass in He or H_2/He mixtures (30 mg BM/pulse; vapor WHSV of 2 h⁻¹).
- Compared acid catalysts: HZSM-5 (**A**) & $\text{Mo-HPA}/\text{TiO}_2$ (**B**).
- Utilized molecular beam mass spectrometry (MBMS) for real-time analysis of products.
- $\text{Mo-HPA}/\text{TiO}_2$ regeneration methods:
 - **Mild Oxidative**, 5 vol% O_2 in He, 425°C, 0.5 h
 - **Severe Oxidative**, 21 vol% O_2 in He, 550°C, 4 h
 - **Reductive**, 100 vol% H_2 , 400°C, 5 h
- Acid site characterization via pyridine adsorption diffuse reflectance Fourier transform infrared spectroscopy (py-DRIFTS).

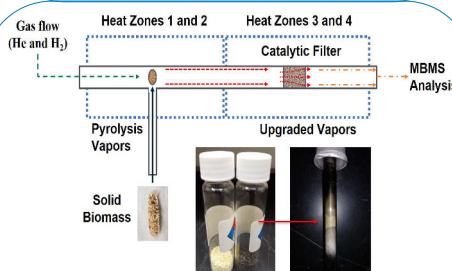


Figure 1. Lab scale pulsed-flow experimental setup showing the horizontal quartz reactor system (upper left) coupled to a molecular beam mass spectrometer (MBMS, right) for real-time analysis of products. Catalyst is shown pre- and post-reaction (coked).

Literature Cited & Acknowledgements

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Results & Discussion

Lab scale pulsed-flow experiments (Figure 2):

- Catalyst **A** produced VGO-soluble BTX and naphthalenes without the need for added H_2 .
- Catalyst **B** produced polyalkyl benzenes/anthracenes in addition to BTX and naphthalenes under reducing conditions (with H_2) → increased non-polarity may enhance VGO-solubility and biogenic carbon incorporation for coprocessing
- Catalyst **B** partially regenerated via mild oxidative and reductive conditions; severe oxidative treatment significantly reduced catalyst activity.
- Catalyst **B**, py-DRIFTS acid site characterization (Figure 3 and Table 1):
 - Addition of Mo-HPA to TiO_2 adds Brønsted acidity
 - Acidity partially retained after regeneration → B/L of ~0.2–0.3 retained post mild regeneration

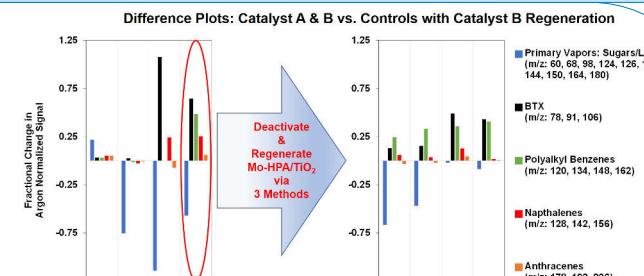
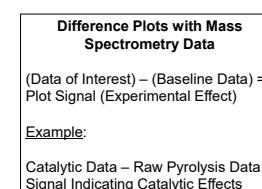


Figure 2. Mass spectral data showing pine pyrolysis upgrading using: **Control** hydrogen (H_2 ; i.e., hydropyrolysis), TiO_2 (titania), **A** HZSM-5 (without H_2), **B** molybdenum heteropolyacid on titania ($\text{Mo-HPA}/\text{TiO}_2$), **C** deactivated $\text{Mo-HPA}/\text{TiO}_2$, **D** severely oxidatively regenerated $\text{Mo-HPA}/\text{TiO}_2$, **E** mildly oxidatively regenerated $\text{Mo-HPA}/\text{TiO}_2$, and **F** reductively regenerated $\text{Mo-HPA}/\text{TiO}_2$.

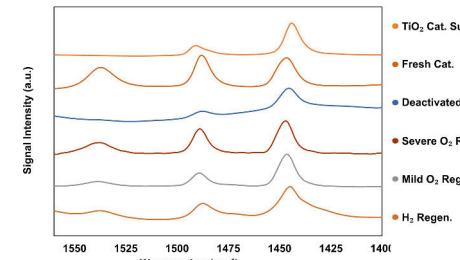


Figure 3. Acid site stability as a function of reaction via pyridine adsorption diffuse reflectance Fourier transform infrared spectroscopy (py-DRIFTS) for pulsed-flow conditions. Modes at ~1447 cm⁻¹ and ~1537 cm⁻¹ are attributed to pyridine coordination with Lewis and Brønsted acid sites, respectively. Mode at ~1490 cm⁻¹ is indicative of both Lewis and Brønsted acid sites.⁴

Table 1: py-DRIFTS Data – Brønsted and Lewis acidity ratios for TiO_2 and $\text{Mo-HPA}/\text{TiO}_2$ pre- and post-regeneration.

Conditions	Bronsted Acidity/Lewis Acidity Ratio (B/L)
TiO_2	-
Fresh $\text{Mo-HPA}/\text{TiO}_2$	1.27
Deactivated $\text{Mo-HPA}/\text{TiO}_2$	0.05
Mild Oxidative Regeneration for $\text{Mo-HPA}/\text{TiO}_2$	0.28
Severe Oxidative Regeneration for $\text{Mo-HPA}/\text{TiO}_2$	0.80
Reductive Regeneration for $\text{Mo-HPA}/\text{TiO}_2$	0.19

Conclusions & Future Work

- $\text{Mo-HPA}/\text{TiO}_2$ selective towards polyalkyl benzenes/anthracenes for potential VGO-solubility enhancement.
- $\text{Mo-HPA}/\text{TiO}_2$ regenerable under reductive and mild oxidative conditions.
- Future work – compare VGO-solubility of products and product speciation for HZSM-5 and $\text{Mo-HPA}/\text{TiO}_2$; assess preconditioned product speciation on coprocessing and/or hydroprocessing.