

# An Adaptive-Mesh-Refinement Based Computational Tool for Simulating Catalysis at Mesoscale

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#### Introduction and Motivation

 Biomass thermochemical conversion and catalytic upgrading are complex multiscale processes.

Mesoscale modeling facilitates:

- Connect molecular and reactor scales
- Investigation of intra-particle transport phenomena
- Complex surface morphologies can significantly affect reactivity
- Extraction of transport-dependent reaction/deactivation kinetics



Ciesielski et al., Wiley Reviews: Energy and Environment, 2018

#### Mesoscale modeling challenges





- Complex morphology of particles
  - High resolutions at interfaces
  - Unstructured mesh generation
- Chemistry
  - Mechanisms from experimental data
- Coking and deactivation physics
  - Dynamic feature resolution
- HPC is required to answer these physics questions

# Objectives

- Develop a Mesoscale modeling tool
  - Gas-solid flows
    - Catalytic upgrading of biomass vapors
  - Porous media flows
  - Scalable on current and future DOE HPC resources
    - use distributed and shared-memory parallelism
      - Acceleration hardware like GPUs
  - Automated meshing of complex geometries
  - Incorporate chemistry/transport coupling
  - Be able to simulate dynamic geometries



*Summit* Supercomputer at Oakridge National Laboratory

https://www.ornl.gov/news/ornllaunches-summit-supercomputer

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# Approach

- Leverage open-source library AMReX\*
  - developed at LBNL/NREL/ANL
  - Designed for upcoming Exascale machines
- AMReX is parallel adaptive-mesh refinement (AMR) library
  - Mainly provides block-structured AMR data structures and linear solvers
  - Partial Differential Equation solvers need to be developed using AMReX data structures
  - Code development in C++ with GPU kernels



Flow around sphere Re=4000

#### **Governing equations**

Compressible Navier-Stokes equations (gas phase)

$$\begin{aligned} \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{U}) &= 0\\ \frac{\partial (\rho \mathbf{U})}{\partial t} + \nabla \cdot (\rho \mathbf{U} \mathbf{U}) &= -\nabla P + \nabla \cdot \bar{\bar{\tau}}\\ \frac{\partial (\rho E)}{\partial t} + \nabla \cdot (\rho E + P) &= \nabla \cdot (k \nabla T) + \nabla \cdot (\bar{\bar{\tau}} \cdot \mathbf{U}) \end{aligned}$$

Species transport and reaction (both gas and solid phase)

$$\frac{\partial c_i}{\partial t} + \nabla \cdot (c_i \mathbf{U}) = \nabla \cdot (D_i \nabla c_i) + \dot{W}_i$$

- AUSM+up\* scheme for low-Mach flows
- Level-set immersed boundary method at the boundaries
- Temperature dependent transport and thermal properties



Reflection based boundary conditions for velocity at the interface

# Chemistry



No.	Reaction	k[m³/(mol.s)] @ T=500ºC
1	$PV + S1 \rightarrow HC + S1$	2.573
2	$PV + S1 \rightarrow CK + S2$	0.456
3	$PV + S2 \rightarrow CK + S3$	0.152
4	PV + S2 → FPN + S2	2.904
5	$\rm HC + S1 \rightarrow CK + S3$	0.507
6	$FPN + S2 \rightarrow CK + S3$	0.006
7	FPN + S2 $\rightarrow$ HC + S2	0.051



- Validated 7 species chemistry for Zeolite catalyst
  - Gas phase primary vapors, products
  - Solid phase Coke and catalyst sites
- Operator splitting approach to couple with transport

# Parallelization strategy



- Boxes (32<sup>3</sup> or 64<sup>3</sup> size) per rank run using either
  - Openmp threads on smaller tiles
  - multiple GPU streams
- Stencil operations executed through asynchronous GPU kernels
  - Inlined functions called from within C++ lambda
- Data movement managed through AMReX
  - Large chunk of unified memory initially allocated
- Currently setup with 1 GPU per MPI rank configuration

### Catalyst particle simulations

Particle Reconstruction











- Directly reconstruct volume fraction field in an AMR mesh
  - X-ray tomography data in the form of MRC/TIFF files
    - Pixel data with a threshold is used to identify solid domain
  - Stereolithography (STL) surface files
    - Ray tracing/Plucker coordinates method to identify solid region

## Catalyst particle simulations





Davison Circulating Riser\* at NREL

- Setup is similar to experiments done at NREL
  - catalytic upgrading of biomass pyrolysis vapors in a DCR reactor
  - Primary vapors in helium background gas
  - 100  $\mu$ m size particle
  - Free stream conditions: P=1 atm., T = 700 K, V = 0.25 m/s
- First, we solve non-reacting flow to steady state

\*Jarvis, Mark W., et al. "Catalytic upgrading of biomass pyrolysis oxygenates with vacuum gas oil using a Davison circulating riser reactor." *Energy & Fuels* 32.2 (2018): 1733-1743.

# Catalyst particle simulations



#### Partially deactivated particle







- Coke formation in the outer porous regions
- Qualitatively matches coked catalyst images
- Hydrocarbon products are transported out of porous region
- Site concentration reduces as coking happens
- Deactivation time-scale ~ 10s of mins
  - Matches experimental data



### **Computational performance**



- Strong scaling observed over 10000 MPI ranks
  - 20% of NREL Supercomputer, Eagle
- OpenMP also shows good scaling on 32x32x32 boxes

# **GPU** performance



- A single GPU provides ~ 10X or more performance compared to a single CPU
- ORNL summit shows superior performance compared to Eagle GPUs
- Summit has 6 GPUs per node compared to 2 GPUs on eagle

# Conclusions and future work

- Conclusions
  - Developed a mesoscale modeling tool with
    - Using AMReX library
    - Adaptive mesh refinement
    - Complex geometry representation
    - Hybrid parallelization on HPC
  - Studied catalysis of biomass pyrolysis vapors over zeolite particle
    - Coking phenomena qualitatively matched imaging
- Future work
  - Performance optimizations on GPU
  - Incorporate heat-transfer effects
  - Other catalysis problems
- Questions/comments email me at Hariswaran.Sitaraman@nrel.gov

#### www.nrel.gov

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![](_page_15_Picture_3.jpeg)