

# Techno-economic analysis and life-cycle assessment of emerging technologies for bioprocessing separations

Lauren Valentino and Jennifer B. Dunn – Argonne National Laboratory Eric C.D. Tan – National Renewable Energy Laboratory Charles J. Freeman – Pacific Northwest National Laboratory William Kubic – Los Alamos National Laboratory Alex Rosenthal – inCTRL Solutions



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#### The challenge: separations

#### TOTAL U.S. ENERGY CONSUMPTION

Separations account for 45 - 55% of **industrial** energy use and 10 - 15% of **TOTAL** energy consumption TOTAL BIOPROCESSING COSTS

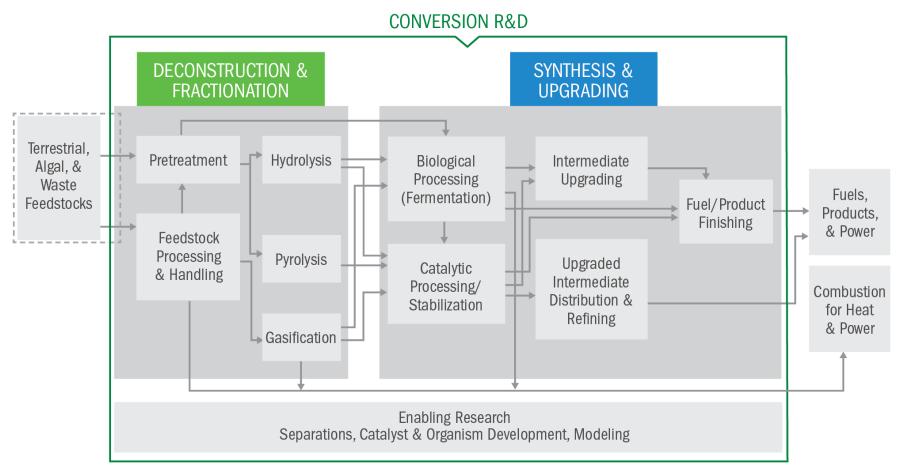
60-80% of BIOPROCESSING COSTS are associated with separations

> Sholl and Lively 2016, Ragauskas et al. 2006





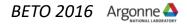
### **Conversion pathways**



Separations are costly and complex regardless of conversion pathway

Challenges are related to upstream and downstream separations

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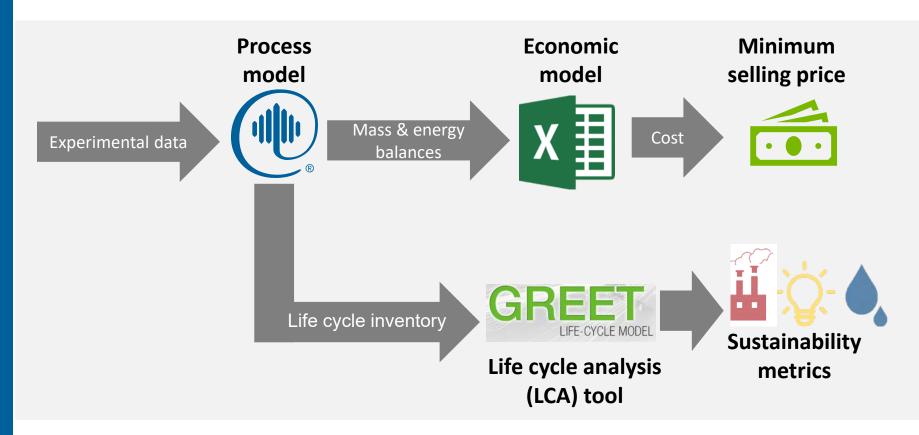


## **Major bioprocessing separation** challenges

Lignin fractionation and valorization	Lignin fractionation enables conversion to valuable co-products that can enhance process economics and sustainability.
Recover carbon from dilute aqueous streams	Increasing carbon efficiency of processes from recovery of valuable co-products can lead to improved process economics.
Remove catalyst poisons from feedstocks and fermentation broth	Poisons and foulants like carbonyls limit the lifetimes of upgrading catalysts and biocatalysts. Selective removal strategies to eliminate them will extend catalyst life and decrease processing costs.
Process intensification	Reducing the number of processing steps associated with separations, including through reactive fermentation and in-situ product recovery, reduce process energy intensity and costs.



## **Integrated analysis approach**



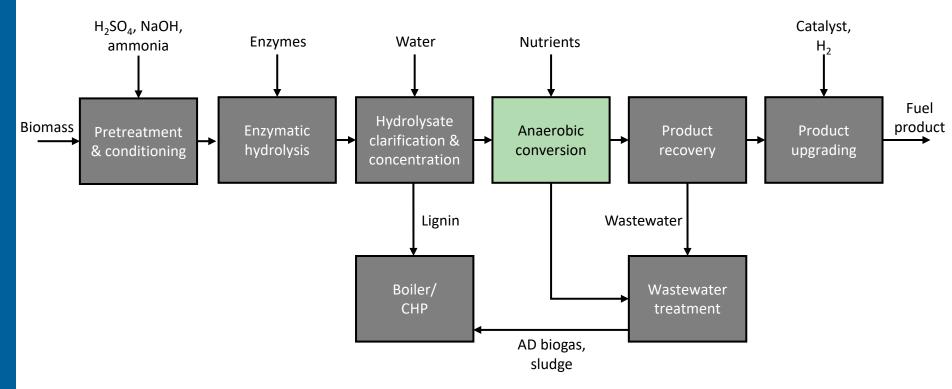
GREET<sup>™</sup>: Greenhouse gases, Regulated Emissions and Energy use in Transportation





## **Analysis for separations strategies**

#### **Biochemical conversion example**



Anaerobic production of carboxylic acids was identified as a strategy to produce biological intermediates that could be further upgraded to a hydrocarbon fuel via chemical catalytic conversion



## **Analysis methodology**

SOT description / Baseline case	State-of-the art commercial technology Establish benchmarks Starting point for model design basis	
Economic viability analysis of both SOT and novel separations	Incorporate innovative technologies Assess how new technologies affect performance and cost Evaluate and develop performance and cost targets	
Environmental impact assessment of both SOT and novel separations	Incorporate innovative technologies Assess how new technologies affect sustainability Evaluate and develop sustainability targets	
Sensitivity analysis	Identify input parameters with high impact on model outputs Establish priorities for technology development	

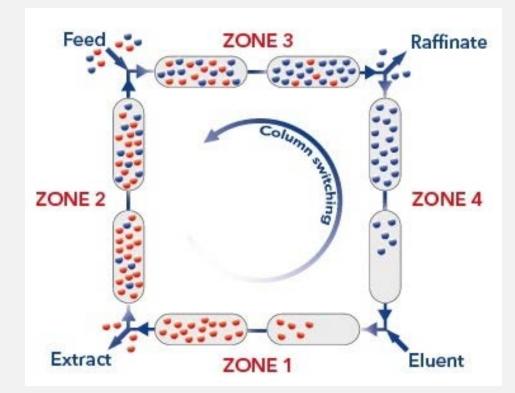




## State of technology – Simulated moving bed

#### Simulated moving bed (SMB)

- SOT for single product isolation
- Limited to A/B separations
- Stationary phase is expensive
- Solvent recycling is complicated in reverse phase



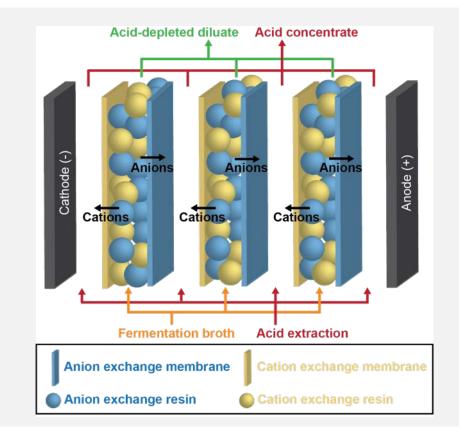




## **Consortium technology -Electrodeionization**

#### **Electrodeionization (EDI)**

- Electrically driven separation
- Ion transport across membranes
- Incorporates ion exchange
- Continuous process with no need for resin regeneration
- In-situ pH control decreases dependence on influent characteristics



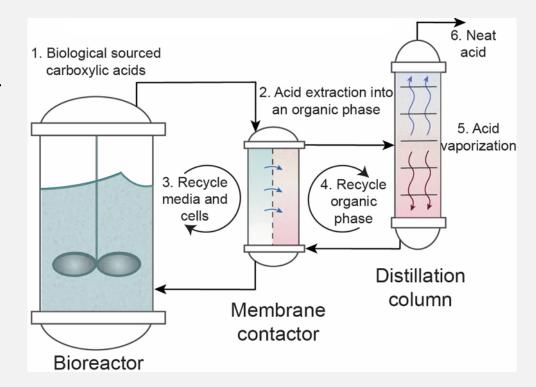




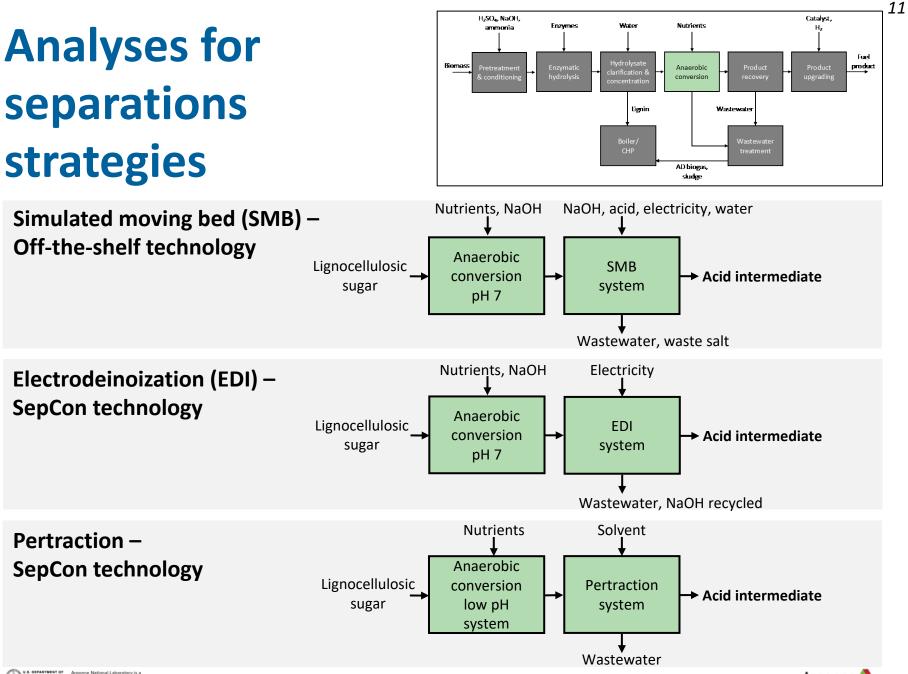
# **Consortium technology – Membrane extraction (pertraction)**

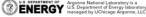
# Pertractive *in-situ* product recovery

- Liquid-liquid membrane extraction system
- Carboxylic acid and solvent separation/recovery via distillation of organic phase
- Increases end-product titer, rate, and yield by avoiding cell inhibition



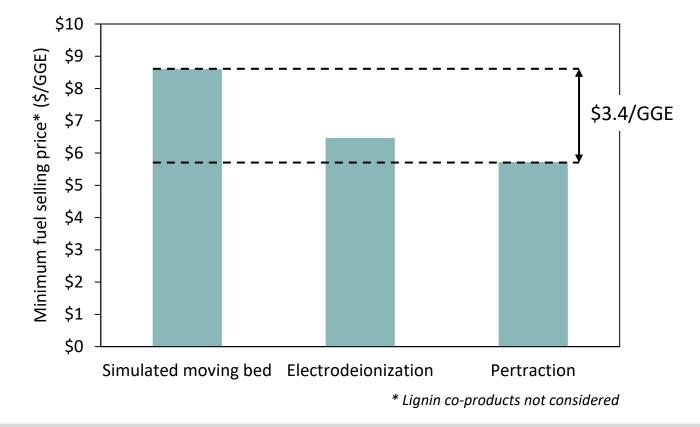








#### **TEA to estimate minimum selling price**



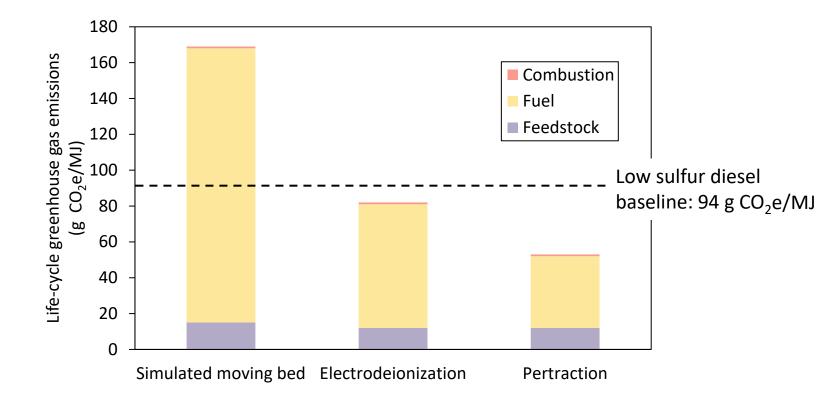
Differences in overall MFSP are attributed to the separation technology

## Compared to baseline technology, EDI and pertractive separations the potential to lower separations costs



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#### LCA to estimate GHG emissions

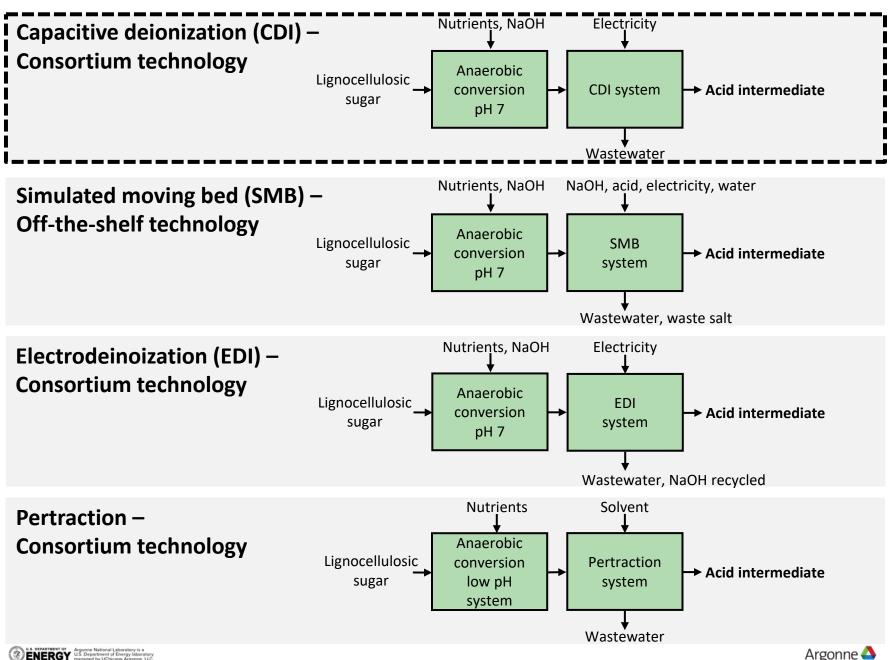


Compared to baseline technology, EDI and pertractive separations result in lower life-cycle GHG emissions for renewable diesel produced

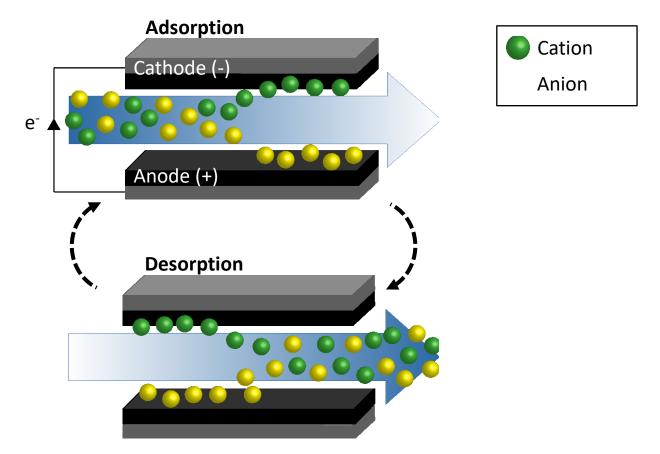
NaOH consumption is key driver for GHG emissions



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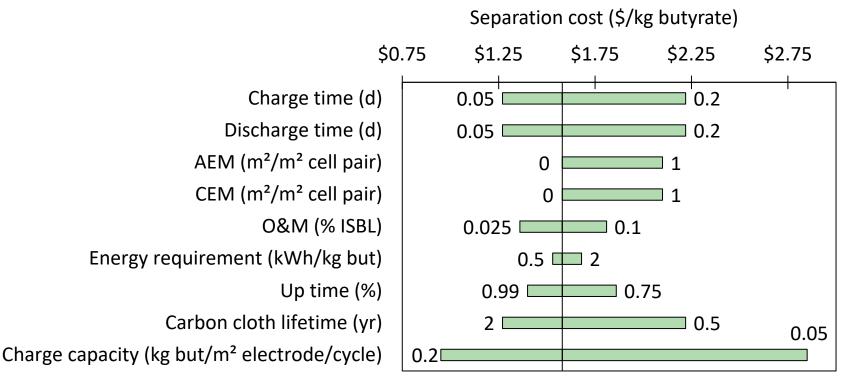
### **Capacitive deionization**



Electric potential drives ion transport towards the electrodes where the ions are stored (adsorption) until the electric potential is reversed or removed resulting in the release of ions (desorption)



# Sensitivity analysis for CDI system performance



Capacity and cycle time (charge + discharge time) are key cost drivers with CDI for separation of butyrate



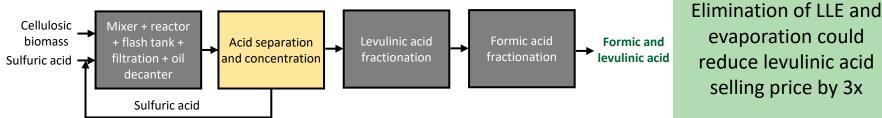


# Other applications for electrochemical technologies in bioprocessing

#### **Conventional furfural process** Furfural Corn bran -Furfural **Furfural** Acetic acid Acetic acid extractive separation separation Sulfuric acid reactor Filter + Sulfuric acid wash separation Sulfuric acid

Electrochemical technology reduces minimum furfural selling price from \$1460/MT to \$1325/MT

#### Levulinic acid production



#### \*Block flow diagrams are simplified





## Integrated analysis to drive R&D

Assess technical, economic, & environmental feasibility of bioproduct/biofuel conversion processes

- Detailed process analysis with rigorous mass and energy balances
- Identify data needs and further R&D need to improve overall cost and efficiency
- Assess environmental impacts (greenhouse gas emissions, fossil fuel consumption, and water consumption)

#### Challenges

- Data availability and quality
- Uncertainty of capital cost for new and novel technologies
- Ensuring rigor of separations process modeling, particularly when considering scale-up





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## Thank you for your attention!

Contact: lvalentino@anl.gov



