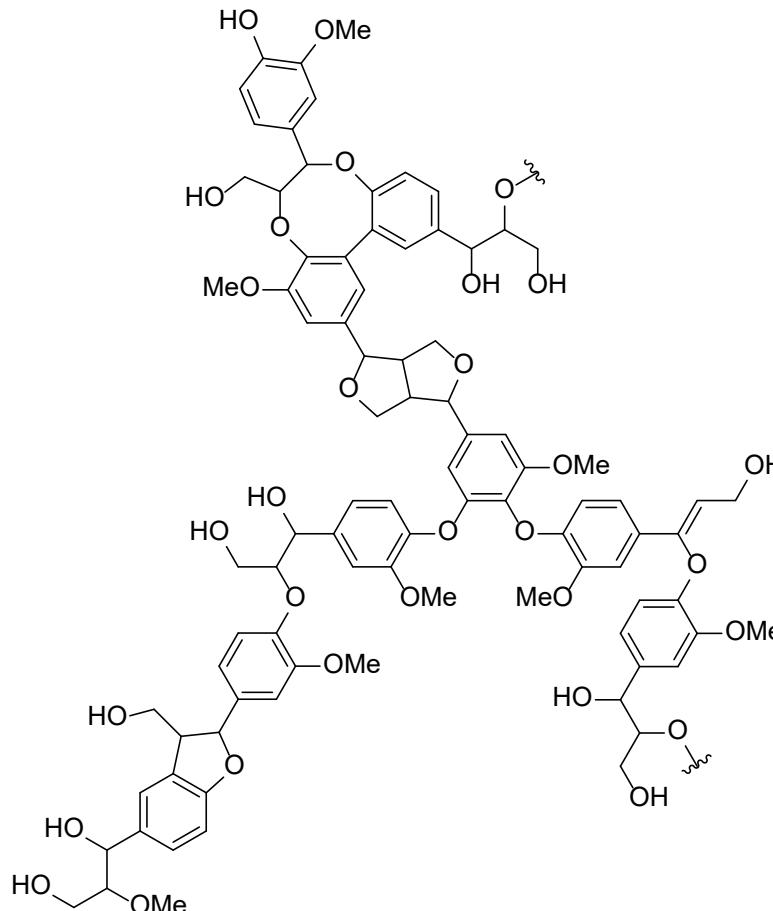




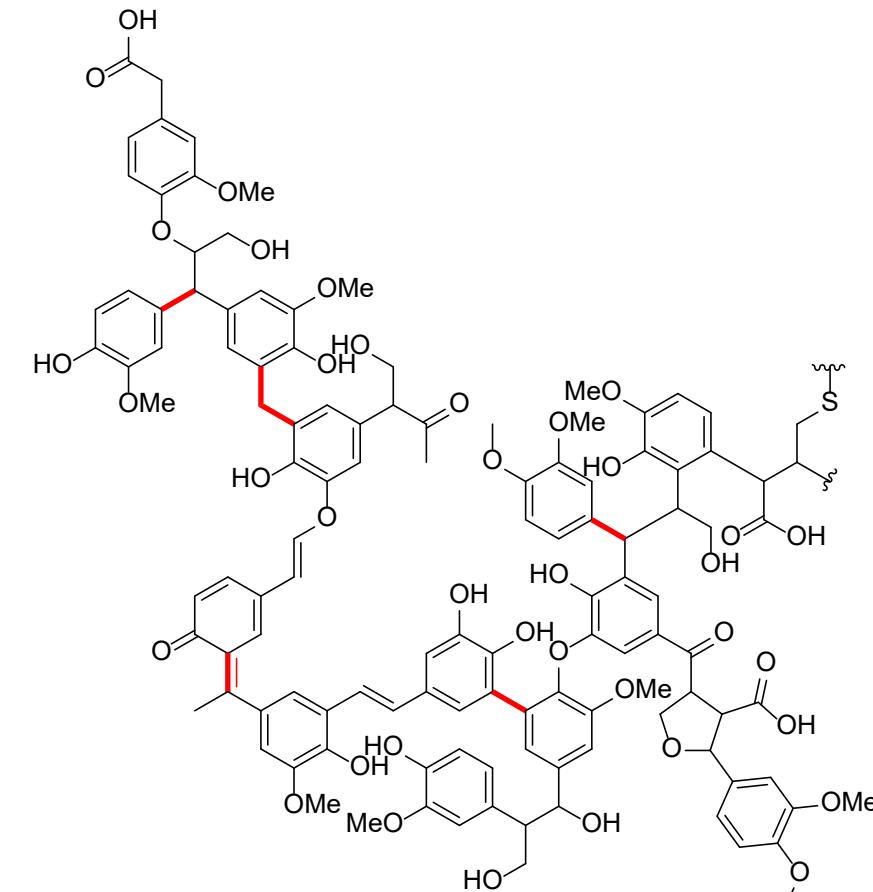
Aromatic monomer production from lignin through
catalytic carbon–carbon bond cleavage

Dr. Chad T. Palumbo
Postdoctoral Researcher

Lignin Valorization: A Case for Depolymerization



softwood native lignin



Kraft lignin

Lignin Valorization: A Case for Depolymerization

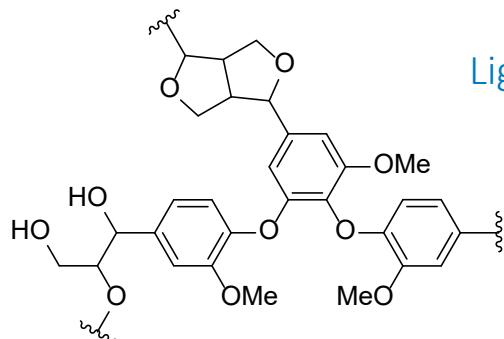
World Consumption – 1.3 million metric tons (growth 1.6% to 2024)

World consumption of lignosulfonates by major region and application—2019 (thousand of metric tons, 100% solids basis)					
	United States	Western Europe	Mainland China	Japan	Total
Dispersants	111	173	103	32	418
Binders and adhesives	118	47	105	22	291
Chemicals and other	12	2	22	5	41
Total	241	222	229	59	751
Percent of total					100%

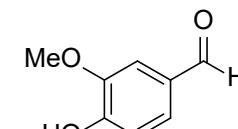
Most end uses already established

Concrete admixtures – largest sector (dispersant) – use has stagnated or even declined due to competition with polycarboxylate-based products

Value (\$/metric ton): liquid 100-300, solid 600-900

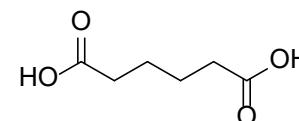


Lignin deconstruction

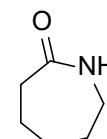


\$229/kg

TMT = thousand metric tons

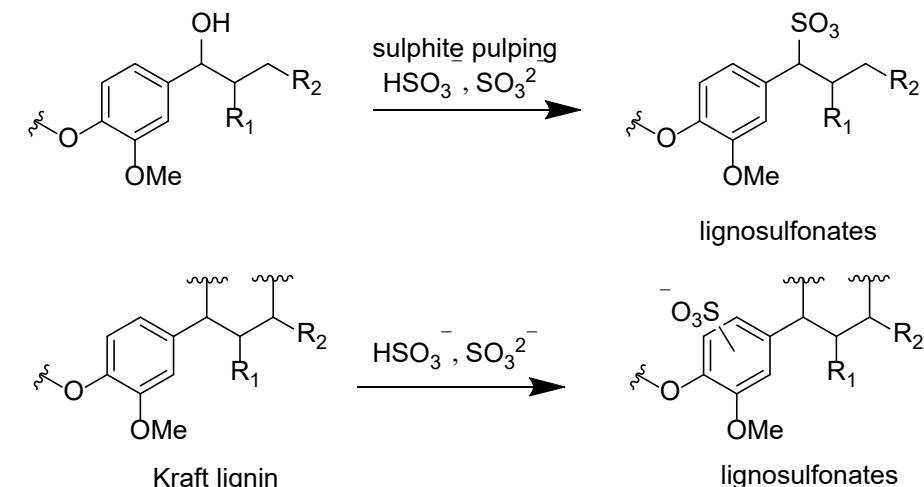


\$1150/metric ton
Market: 3000 TMT



\$1400/metric ton
Market: 6000 TMT

Applications of Lignin – Lignosulfonates



ChemSusChem 2017, 10, 1861–1877

Source: IHS Markit

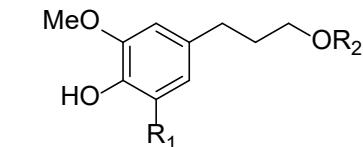
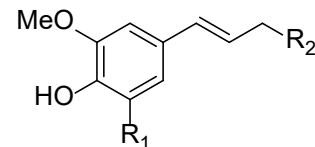
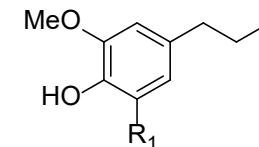
Theoretical Yields of Monomers Through C–O Bond Cleavage Possible

Lignin First Biorefinery: active stabilization approaches that solubilize lignin from native lignocellulosic biomass while avoiding condensation reactions that lead to more recalcitrant lignin polymers

Energy Environ. Sci., 2021, **14**, 262-292



Reductive catalytic fractionation
C–O (Aryl ether) bond cleavage

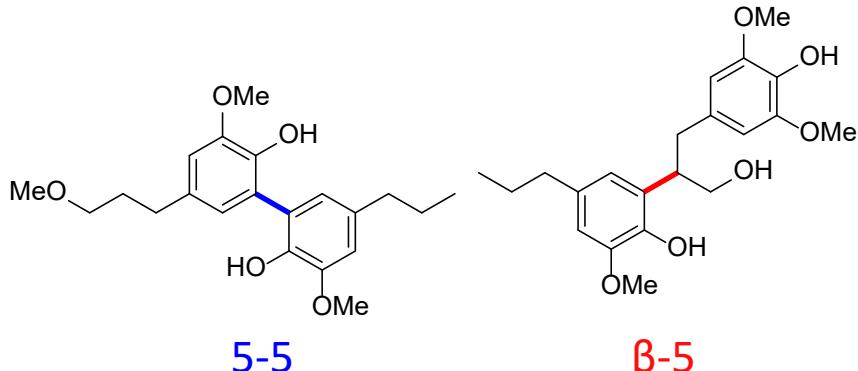


$R_1 = H, OMe; R_2 = OH, OMe$

Monomers

Theoretical Yields of Monomers Obtained: 20-40 wt%

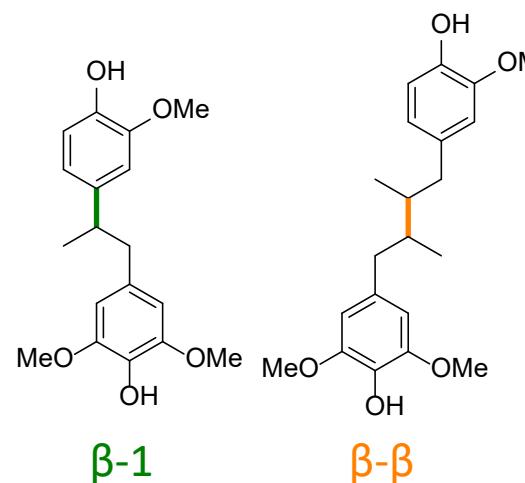
Dimers



5-5

β -5

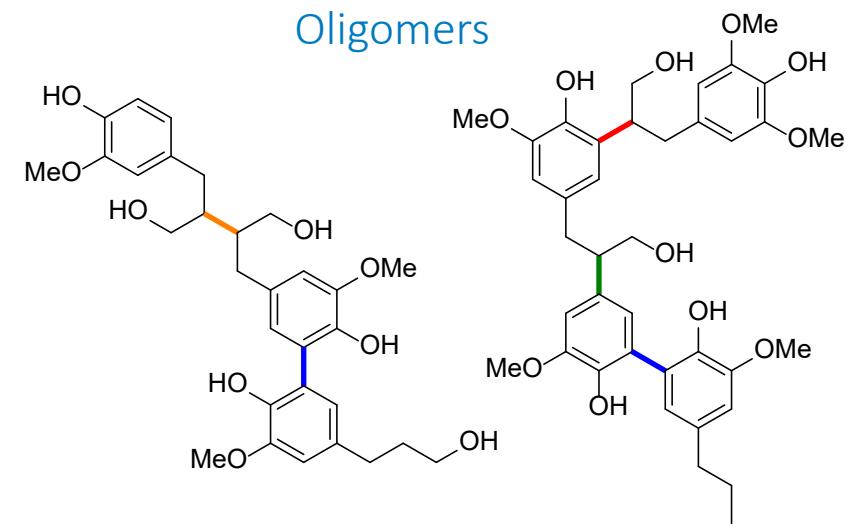
15-20 wt%



β -1

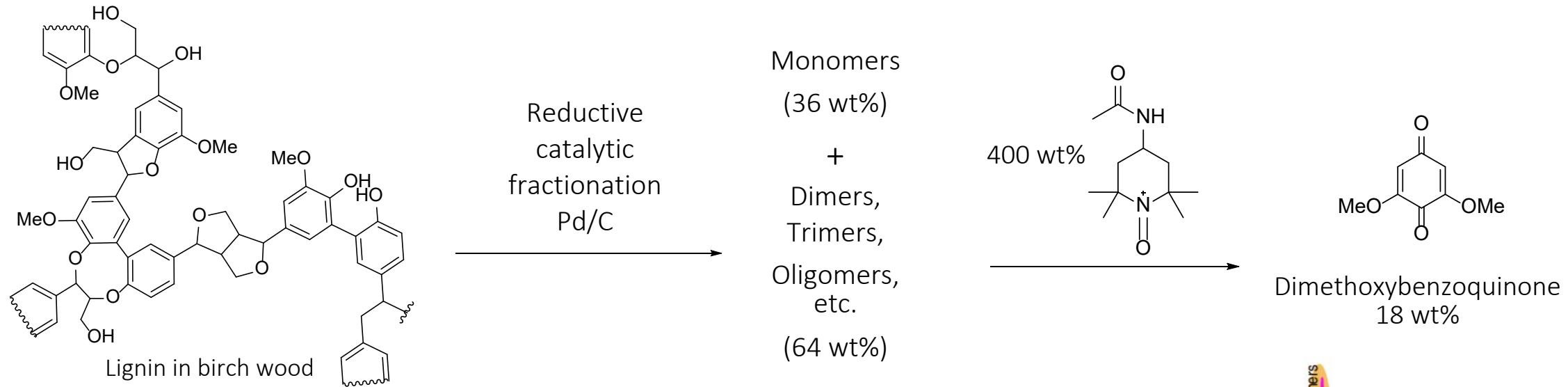
β - β

Oligomers



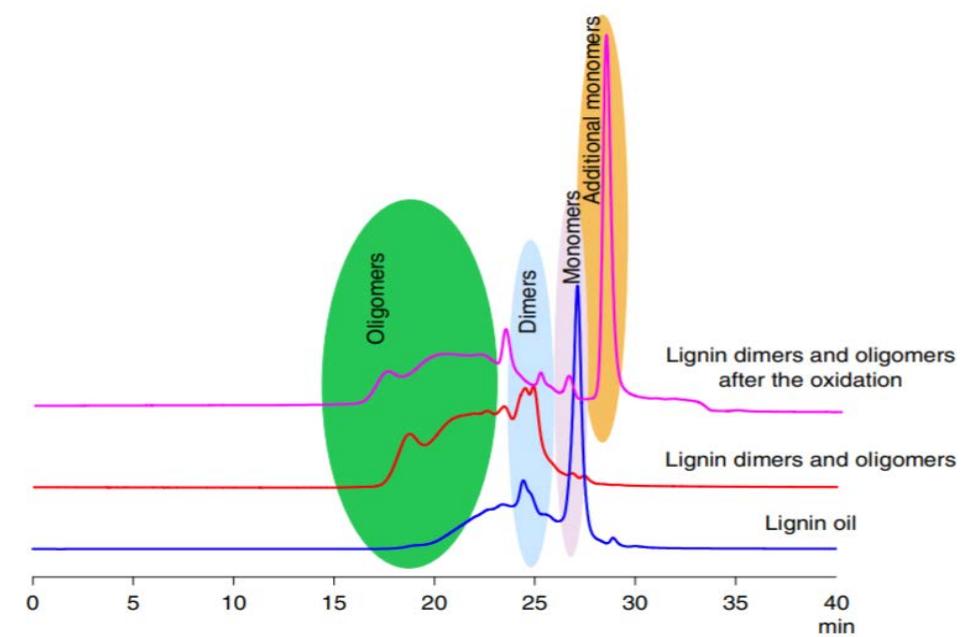
20-40 wt%

Only One Report of C–C Bond Cleavage of RCF Oligomers



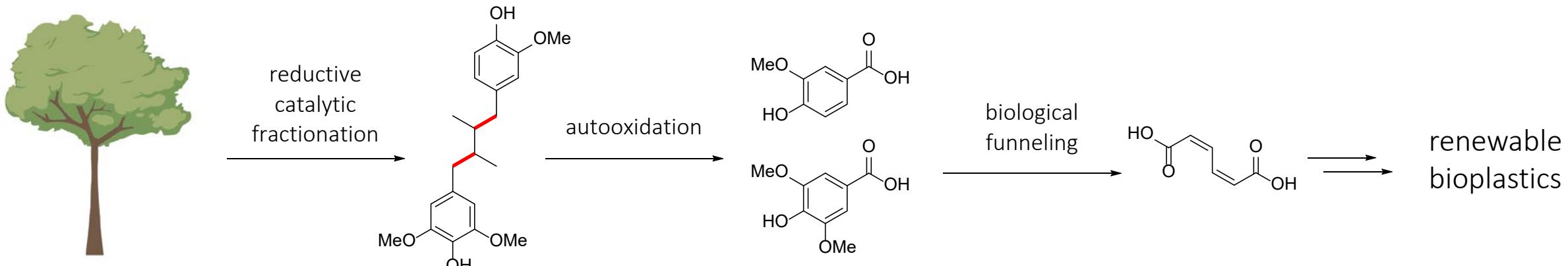
State of the Art:

- Performed with 400 wt% of oxidant
- Oxidant can be subsequently regenerated electrochemically
- Exploits the reactivity of phenols for C–C cleavage

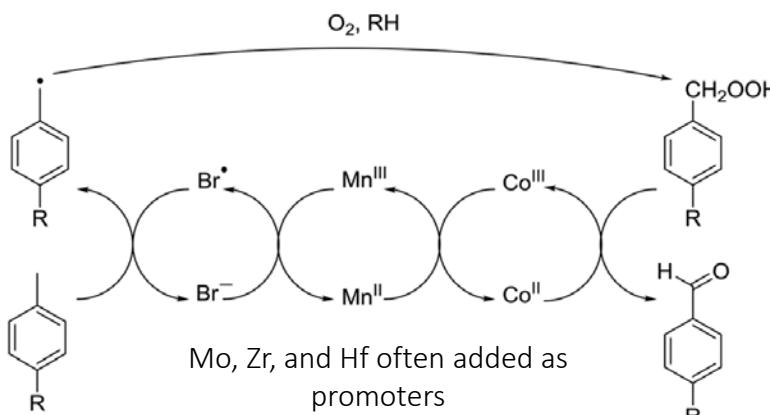


Can We Cleave C–C Bonds Catalytically into Bioavailable Products?

Our Overall Objective

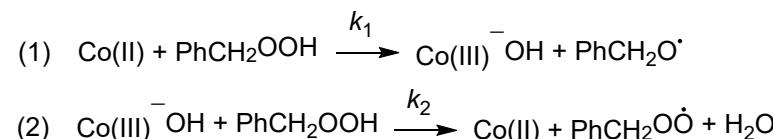


MC Process Simplified Scheme

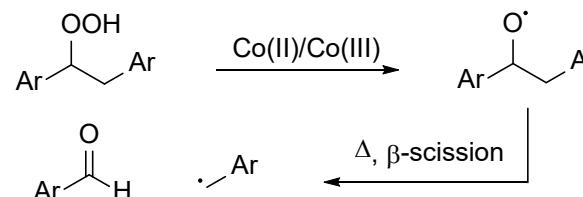


Partenheimer, W. *Catal. Today*, 1995, 23, 69–158

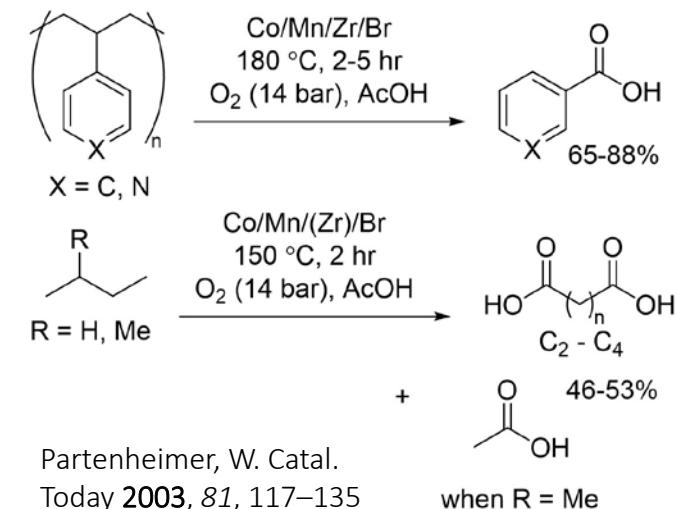
Haber-Weiss Cycle



C–C Bond Cleavage

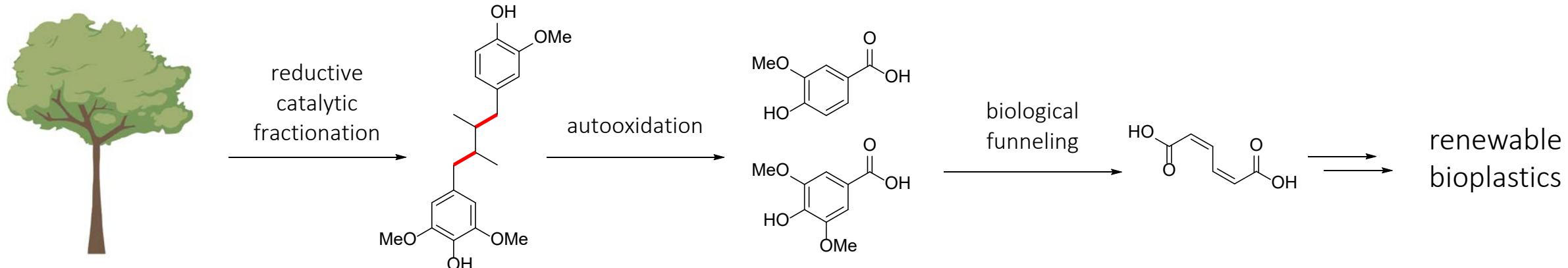


Precedent on C–C Bond Cleavage

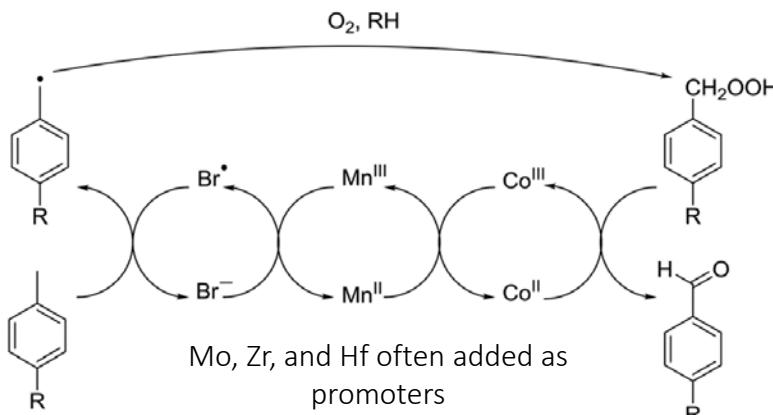


Can We Cleave C–C Bonds Catalytically into Bioavailable Products?

Our Overall Objective

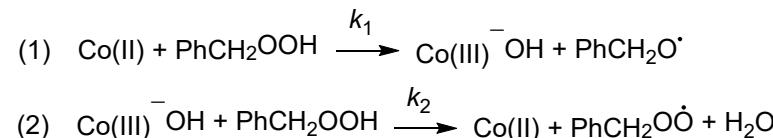


MC Process Simplified Scheme

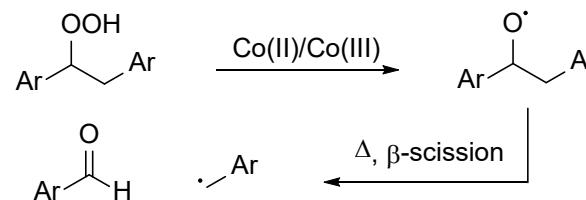


Partenheimer, W. *Catal. Today*, **1995**, 23, 69-158

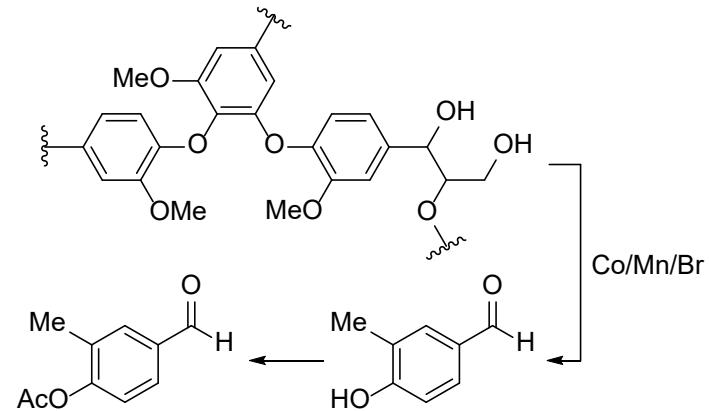
Haber-Weiss Cycle



C–C Bond Cleavage



MC Catalyst on Lignin



Partenheimer, W. *Adv. Synth. Catal.* **2009**, *351*, 456–466;
Clatworthy, E. B. *et al.* *Catal. Sci. Technol.* **2019**, *9*, 384-397.

Can We Cleave C–C Bonds with a Manganese Catalyst?

Ranking of Heterogeneous Catalysts Metals by Their Greenness

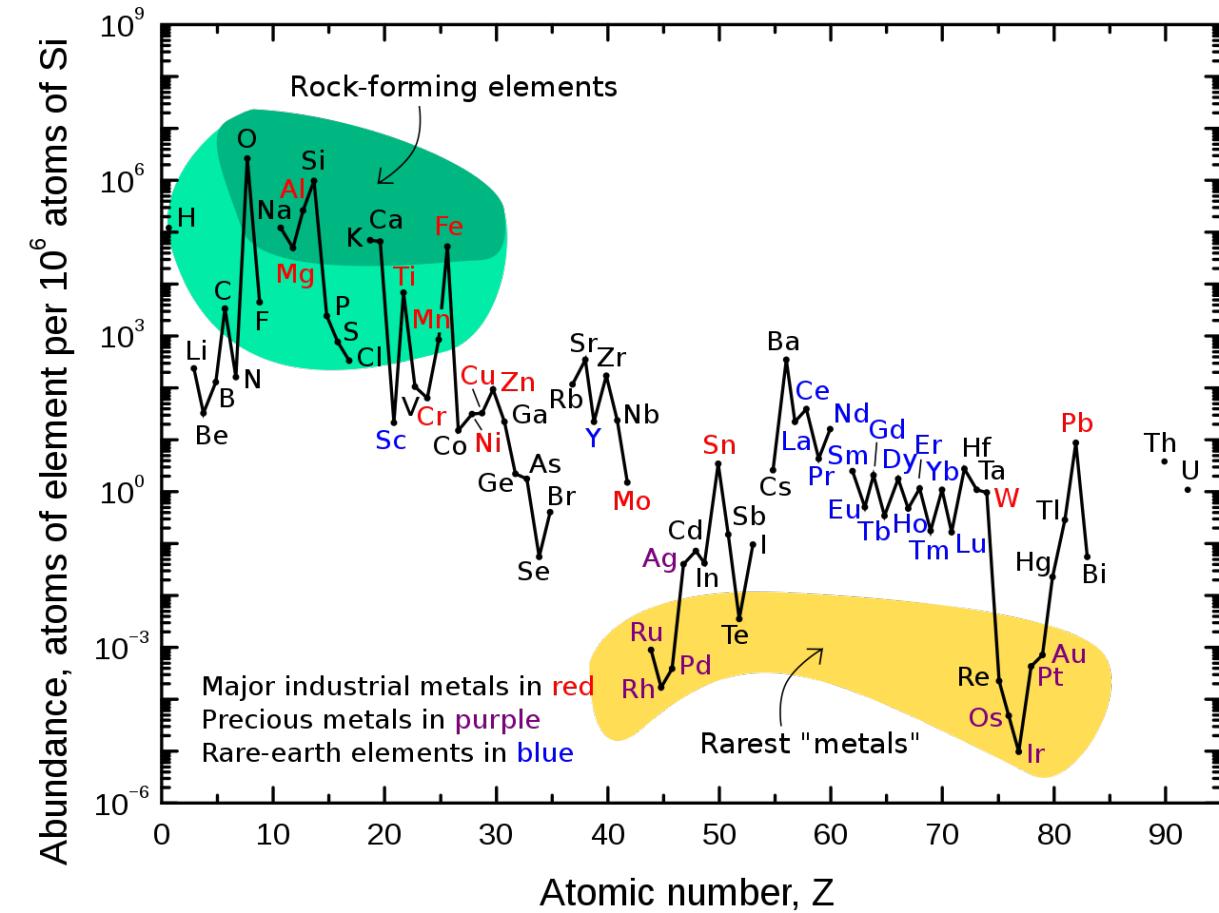
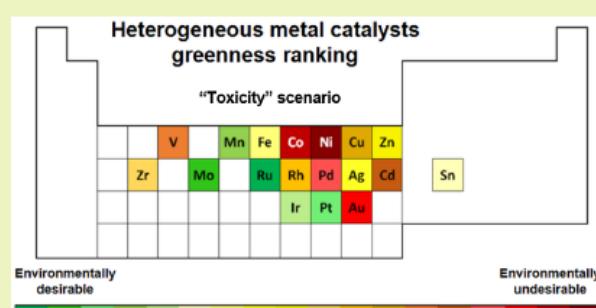
Marta Bystrzanowska,[†] Petko Petkov,[‡] and Marek Tobiszewski^{*†}

[†]Department of Analytical Chemistry, Faculty of Chemistry, Gdańsk University of Technology (GUT), 11/12 G. Narutowicza St., 80-233 Gdańsk, Poland

[‡]Faculty of Chemistry and Pharmacy, University of Sofia, J. Bourchierblvd. 1, 1164 Sofia, Bulgaria

Supporting Information

ABSTRACT: Catalysis is a very important process in industry and laboratory practices, especially from the point of green chemistry principles. However, the eco-friendly character of heterogeneous catalysts containing transition-metal components has not yet been evaluated. Therefore, we performed a comprehensive assessment of 18 heterogeneous metal catalysts (Pd, Pt, V, Co, Ni, Mo, Ru, Mn, Au, Cu, Cd, Zr, Fe, Rh, Ir, Sn, Zn, Ag) using a multicriteria decision analysis approach. The ranking of alternatives according to relevant criteria, such as the toxicity of pure metals and metal salts toward fish, *Daphnia magna*, and algae/plants, metal toxicity toward rats via ingestion, carcinogenicity, the endangerment degree of metals, the boiling point and energy for atom detachment (estimated as metal–metal bond strength in diatomic transition-metal units), and the classification of elemental impurities according to the International Conference on Harmonization, and their degree of importance are presented. Life cycle assessment (LCA)-related parameters of metals have been also included. The assessment showed ruthenium, iron, and molybdenum as the most favorable alternatives, in contrast to nickel, cobalt, and rhodium. Results of environmental evaluation strictly depend on the chosen scenario of assessment, in terms of toxicity, endangered elements, or LCA. Sensitivity analyses toward variations in input data and applied weights prove that the results are reliable. Multicriteria decision analysis can be successfully applied in metal catalyst evaluation for particular case.



Can We Cleave C–C Bonds with a Manganese Catalyst?



Cite This: ACS Sustainable Chem. Eng. 2019, 7, 18434–18443

Research Article

pubs.acs.org/journal/ascecg

Ranking of Heterogeneous Catalysts Metals by Their Greenness

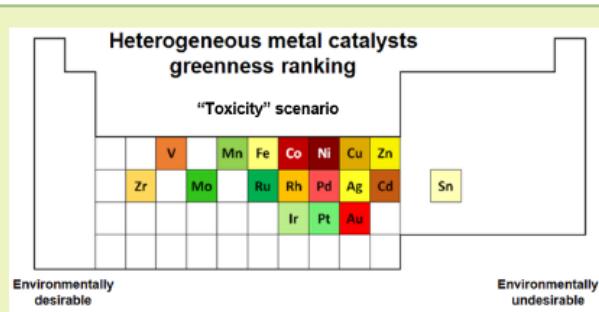
Marta Bystrzanowska,[†] Petko Petkov,[‡] and Marek Tobiszewski^{*†}

[†]Department of Analytical Chemistry, Faculty of Chemistry, Gdańsk University of Technology (GUT), 11/12 G. Narutowicza St., 80-233 Gdańsk, Poland

[‡]Faculty of Chemistry and Pharmacy, University of Sofia, J. Bourchierblvd. 1, 1164 Sofia, Bulgaria

Supporting Information

ABSTRACT: Catalysis is a very important process in industry and laboratory practices, especially from the point of green chemistry principles. However, the eco-friendly character of heterogeneous catalysts containing transition-metal components has not yet been evaluated. Therefore, we performed a comprehensive assessment of 18 heterogeneous metal catalysts (Pd, Pt, V, Co, Ni, Mo, Ru, Mn, Au, Cu, Cd, Zr, Fe, Rh, Ir, Sn, Zn, Ag) using a multicriteria decision analysis approach. The ranking of alternatives according to relevant criteria, such as the toxicity of pure metals and metal salts toward fish, *Daphnia magna*, and algae/plants, metal toxicity toward rats via ingestion, carcinogenicity, the endangerment degree of metals, the boiling point and energy for atom detachment (estimated as metal–metal bond strength in diatomic transition-metal units), and the classification of elemental impurities according to the International Conference on Harmonization, and their degree of importance are presented. Life cycle assessment (LCA)-related parameters of metals have been also included. The assessment showed ruthenium, iron, and molybdenum as the most favorable alternatives, in contrast to nickel, cobalt, and rhodium. Results of environmental evaluation strictly depend on the chosen scenario of assessment, in terms of toxicity, endangered elements, or LCA. Sensitivity analyses toward variations in input data and applied weights prove that the results are reliable. Multicriteria decision analysis can be successfully applied in metal catalyst evaluation for particular case.



Bystrzanowska, M. et al. ACS Sustainable Chem. Eng. 2019, 7, 18343-18443.

Cobalt – \$34,800 / ton
Manganese – \$1,800 / ton

Wood Mackenzie Group, Dec 2020

50 million tons of lignin produced annually in industry

Gosselink, R.J.A. et al. *Ind. Crops Prod.* 2004, 20, 121–129.

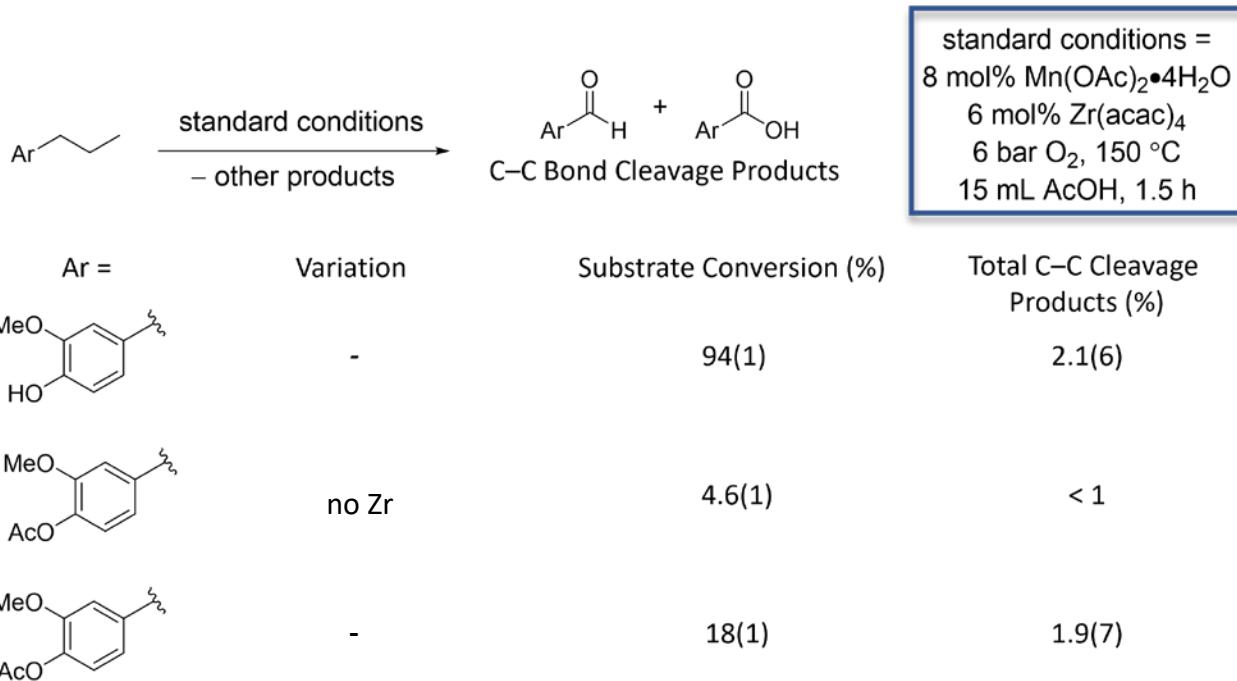
29,400 tons Cobalt

27,400 tons Manganese

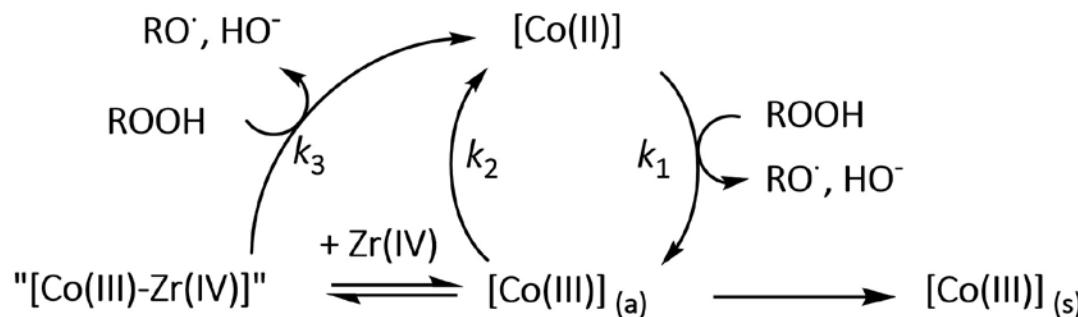
\$1.02 billion / year Cobalt
\$49.3 million / year Manganese

Our aim is to achieve lignin deconstruction to aromatic monomers using a Mn-based catalyst system

Methyl Protection and Zirconium Cocatalyst for Successful C–C Cleavage



How Does Zirconium Promote Co/Mn-catalyzed Autoxidation



Literature on Cobalt / Zirconium Solution Kinetics

Benson, D. et al. *Discussion Farad. Soc.* **1960**, *29*, 60-72

Steinmetz, G.R. et al. *J. Mol. Cat.* **1988**, *49*, L39-L42.

Gould, E. S. et al. *J. Am. Chem. Soc.* **1973**, *95*, 5198-5204.

Hermans, I. et al. *Chem. Eur. J.* **2010**, *16*, 13226-13235.

Jones, G. H. et al. *J. Chem. Soc., Chem Commun.* **1979**, 536-537.

Kochi, J. K. et al. *J. Inorg. Nucl. Chem.* **1971**, *34*, 4101-4109; and refs therein.

Chester, A. W. et al. *J. Catal.* **1977**, *46*, 308-319.

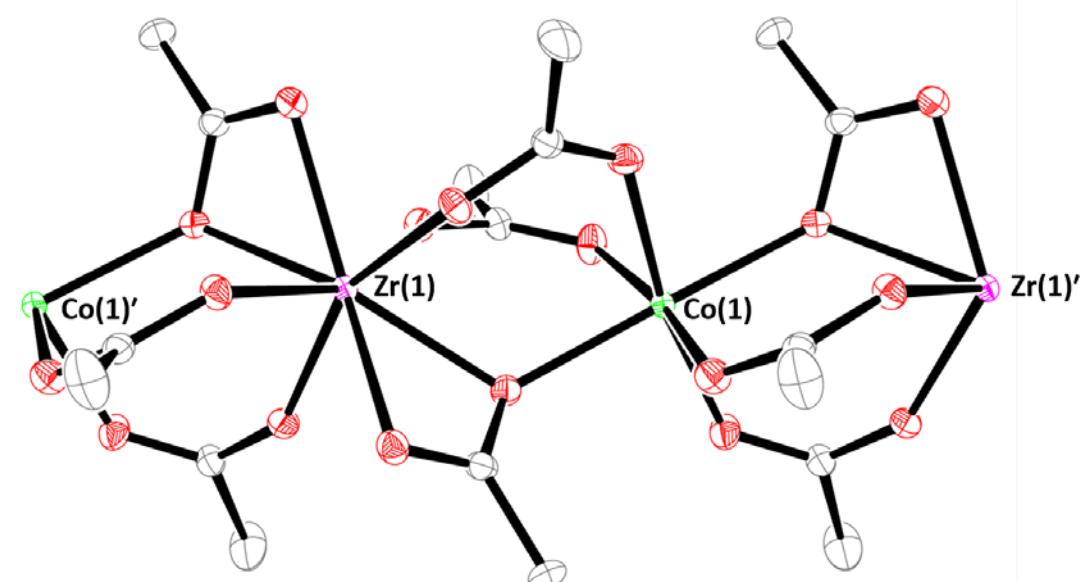
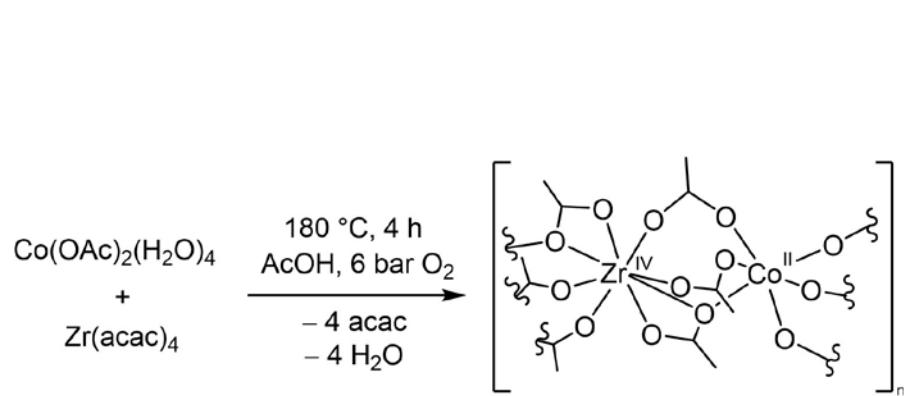
Partenheimer, W. et al. *J. Mol. Catal. Chem.* **2001**, *174*, 29-33.

Partenheimer, W. J. *Mol. Catal. Chem.* **2003**, *206*, 105-119.

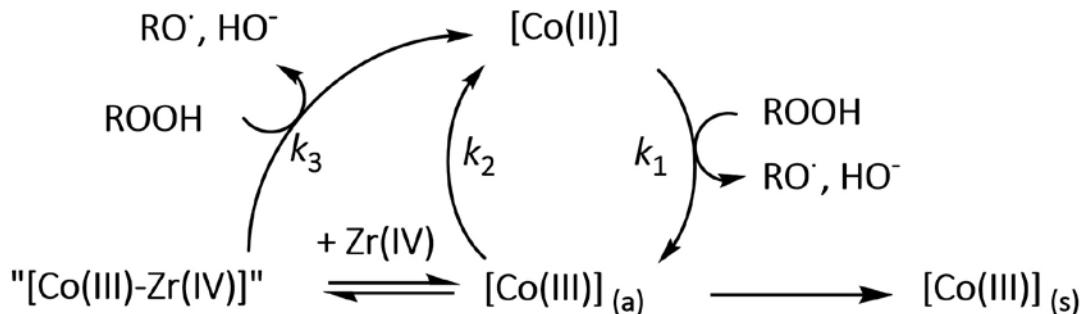
Partenheimer, W. J. *Mol. Catal. Chem.* **2003**, *206*, 131-144.

Zuo, X. et al. *Ind. Eng. Chem. Res.* **2008**, *47*, 546-552.

Partenheimer, W. et al. *Adv. Synth. Catal.* **2001**, *343*, 102-111.



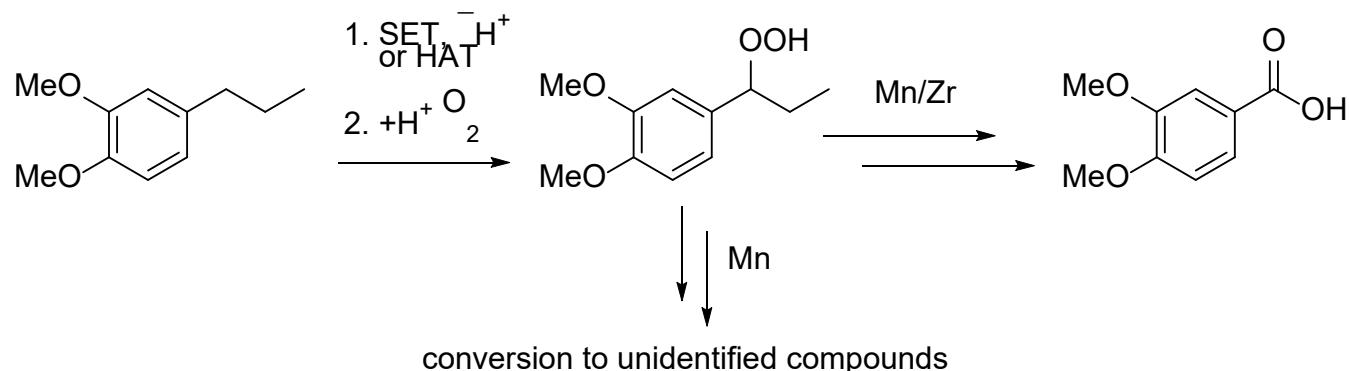
How Does Zirconium Promote Co/Mn Autoxidation



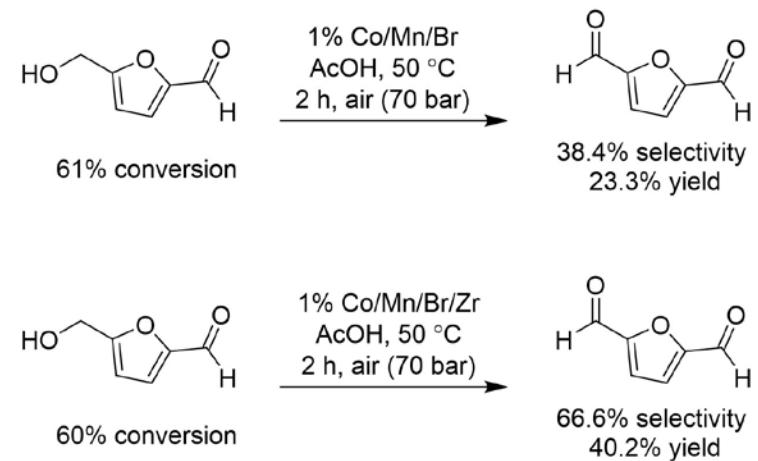
Literature on Cobalt / Zirconium Solution Kinetics

- Benson, D. et al. *Discussion Farad. Soc.* **1960**, 29, 60-72.
Steinmetz, G.R. et al. *J. Mol. Cat.* **1988**, 49, L39-L42.
Gould, E. S. et al. *J. Am. Chem. Soc.* **1973**, 95, 5198-5204.
Hermans, I. et al. *Chem. Eur. J.* **2010**, 16, 13226-13235.
Jones, G. H. et al. *J. Chem. Soc., Chem Commun.* **1979**, 536-537.
Kochi, J. K. et al. *J. Inorg. Nucl. Chem.* **1971**, 4101-4109; and refs therein.
Chester, A. W. et al. *J. Catal.* **1977**, 46, 308-319.
Partenheimer, W. et al. *J. Mol. Catal. Chem.* **2001**, 174, 29-33.
Partenheimer, W. J. *Mol. Catal. Chem.* **2003**, 206, 105-119.
Partenheimer, W. J. *Mol. Catal. Chem.* **2003**, 206, 131-144.
Zuo, X. et al. *Ind. Eng. Chem. Res.* **2008**, 47, 546-552.
Partenheimer, W. et al. *Adv. Synth. Catal.* **2001**, 343, 102-111.

Zirconium allows competitive conversion to carboxylic acid products as opposed to unidentified ones



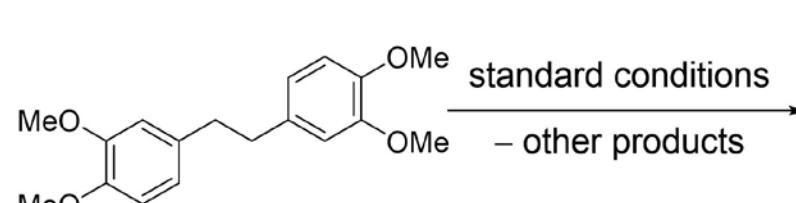
Effect of Zr on Selectivity



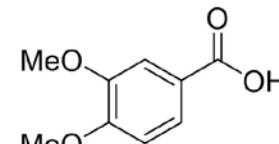
Partenheimer, W.; Grushin, V. V. *Adv. Synth. Catal.* **2001**, 343, 102-111.

Demonstration of C–C Bond Cleavage on Model Dimers

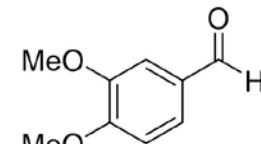
β -1



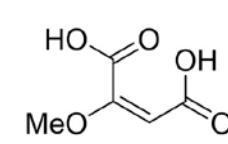
100% conversion



29(3)%



2(2)%

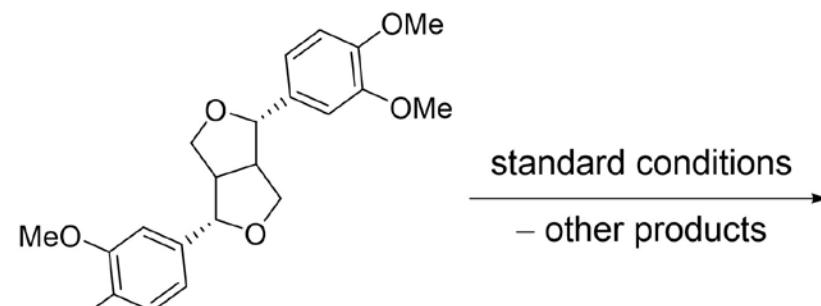


4.4(4)%

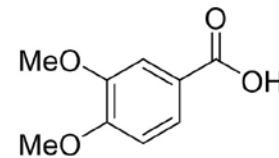
standard conditions =
8 mol% Mn(OAc)₂•4H₂O
6 mol% Zr(acac)₄
6 bar O₂, 150 °C
15 mL AcOH, 1.5 h

total yield = 35(4) mol%; total C–C cleavage monomers = 35(4) mol%

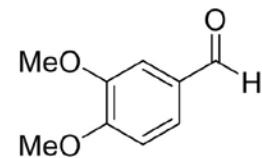
β - β



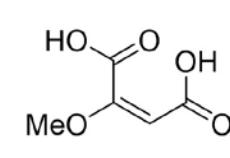
100% conversion



37(2)%



4.4(1)%

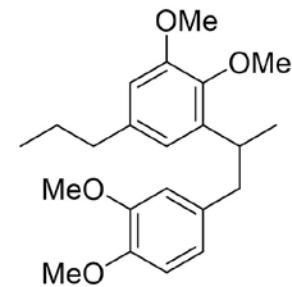


2.9(2)%

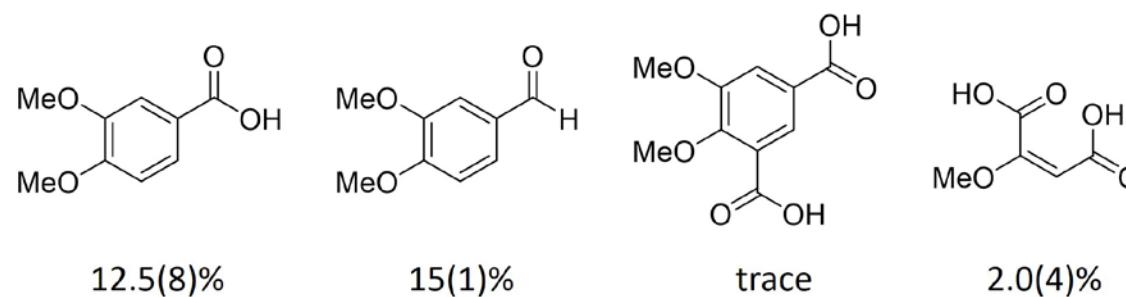
total yield = 45(2) mol%; total C–C cleavage monomers = 45(2) mol%

Demonstration of C–C Bond Cleavage on Model Dimers

β-5



standard conditions
– other products

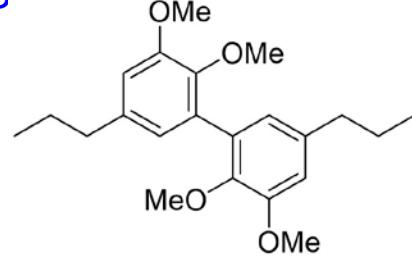


100% conversion

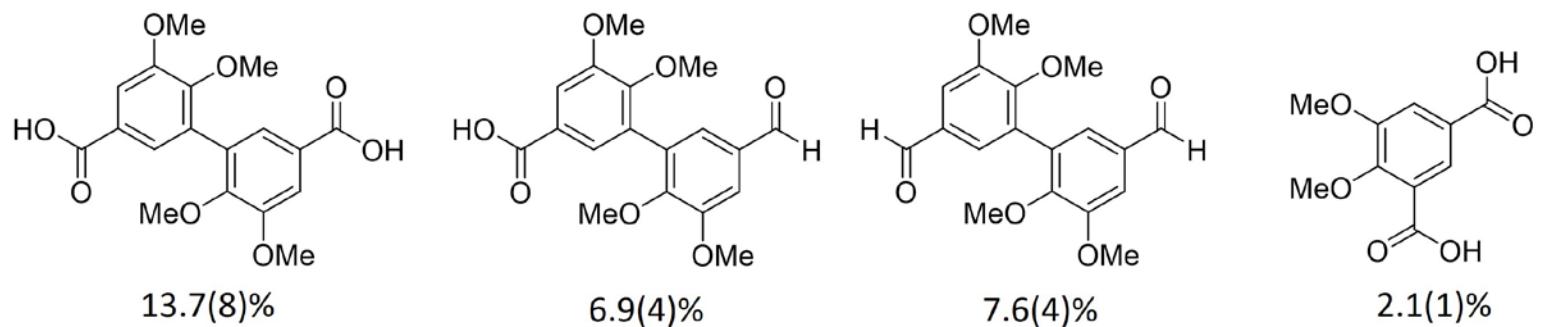
standard conditions =
8 mol% Mn(OAc)₂•4H₂O
6 mol% Zr(acac)₄
6 bar O₂, 150 °C
15 mL AcOH, 1.5 h

total yield = 30(1) mol%; total C–C cleavage monomers = 30(1) mol%

5-5



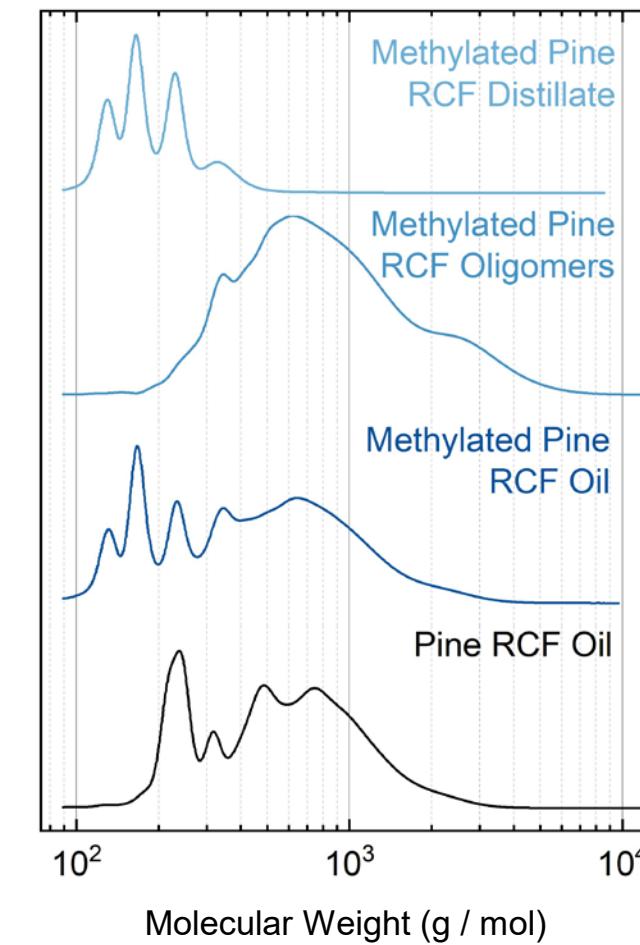
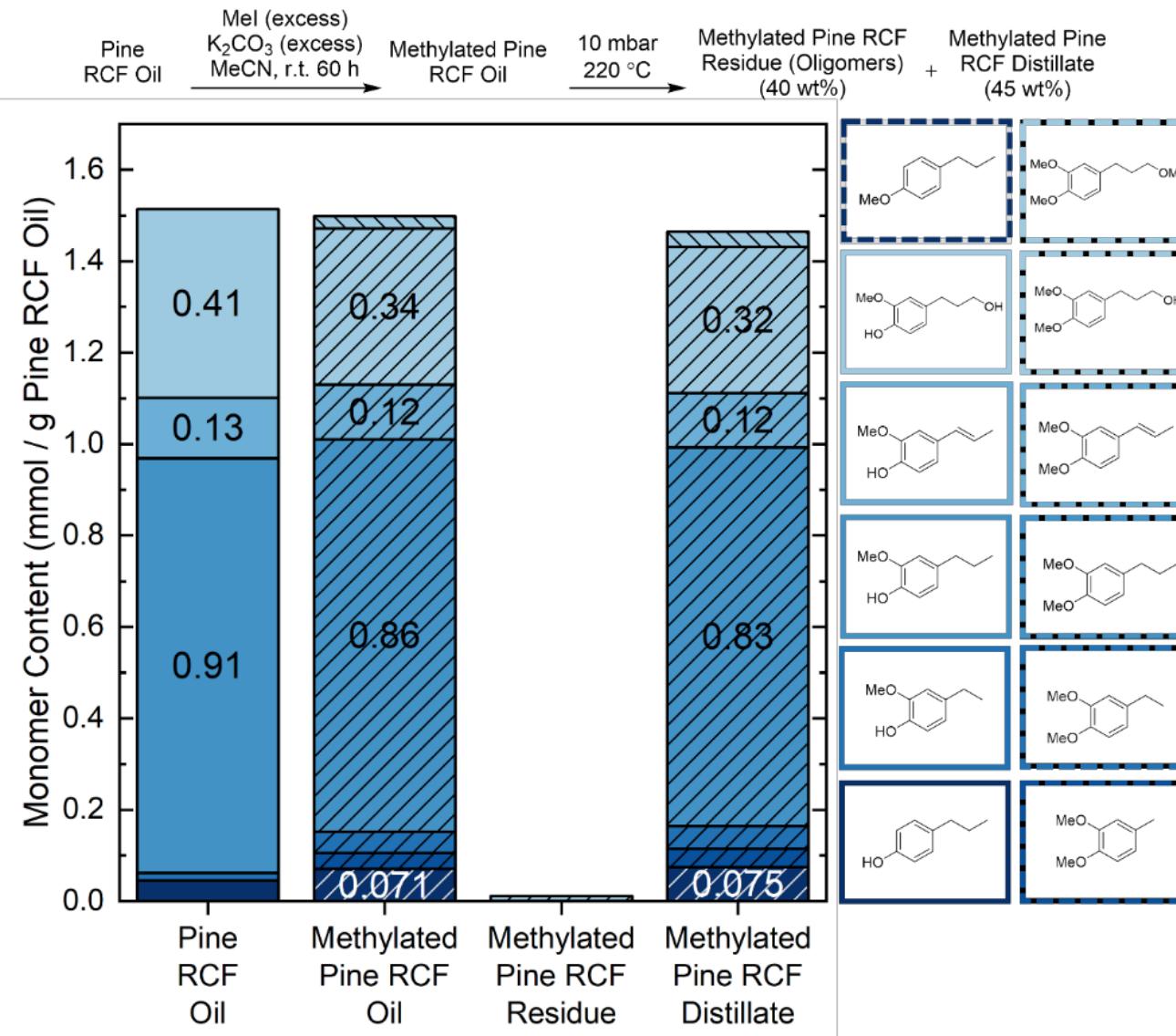
standard conditions
– other products



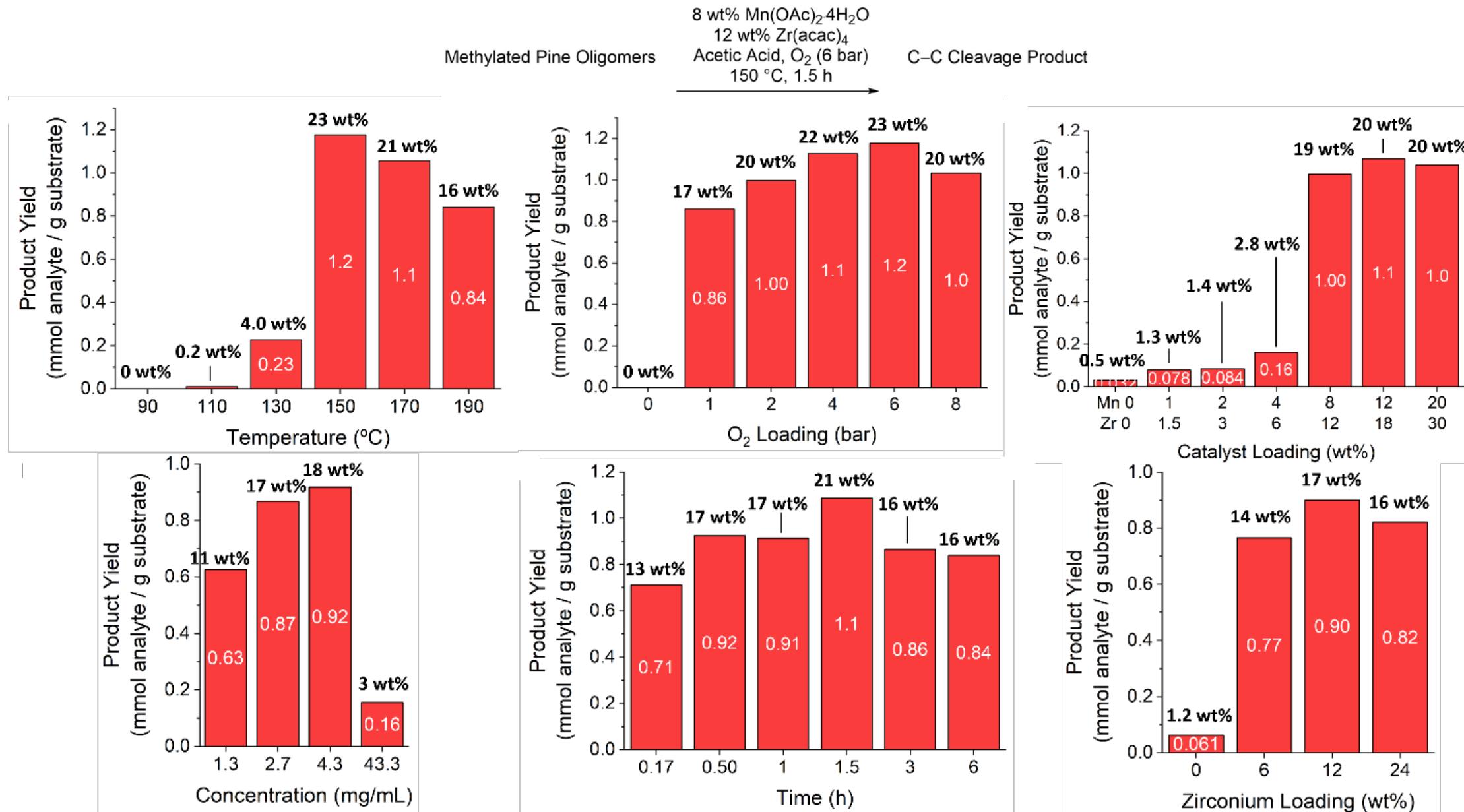
100% conversion

total yield = 30(1) mol%; total C–C cleavage monomers = 2.1(1) mol%

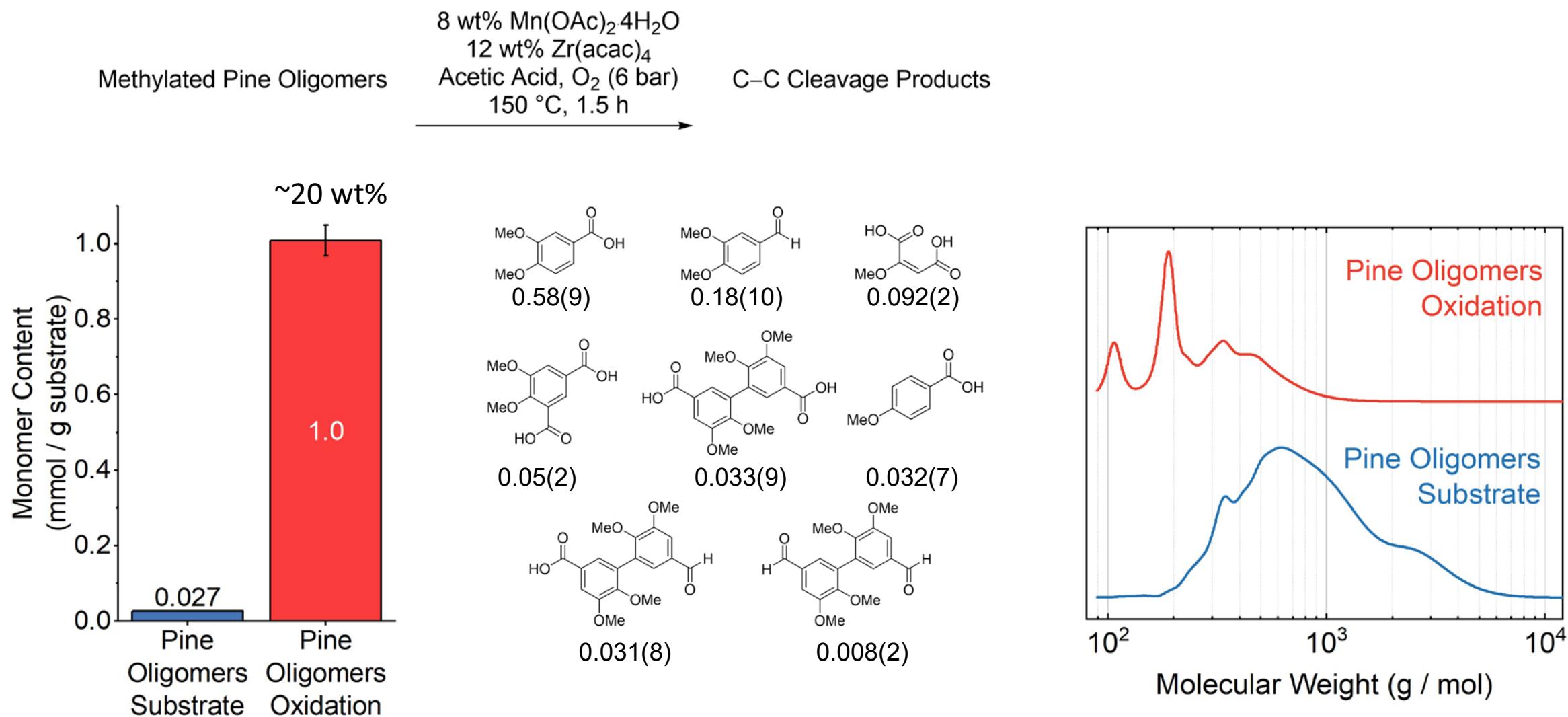
Pine Oligomer Substrate Prepared by Methylation and Distillation



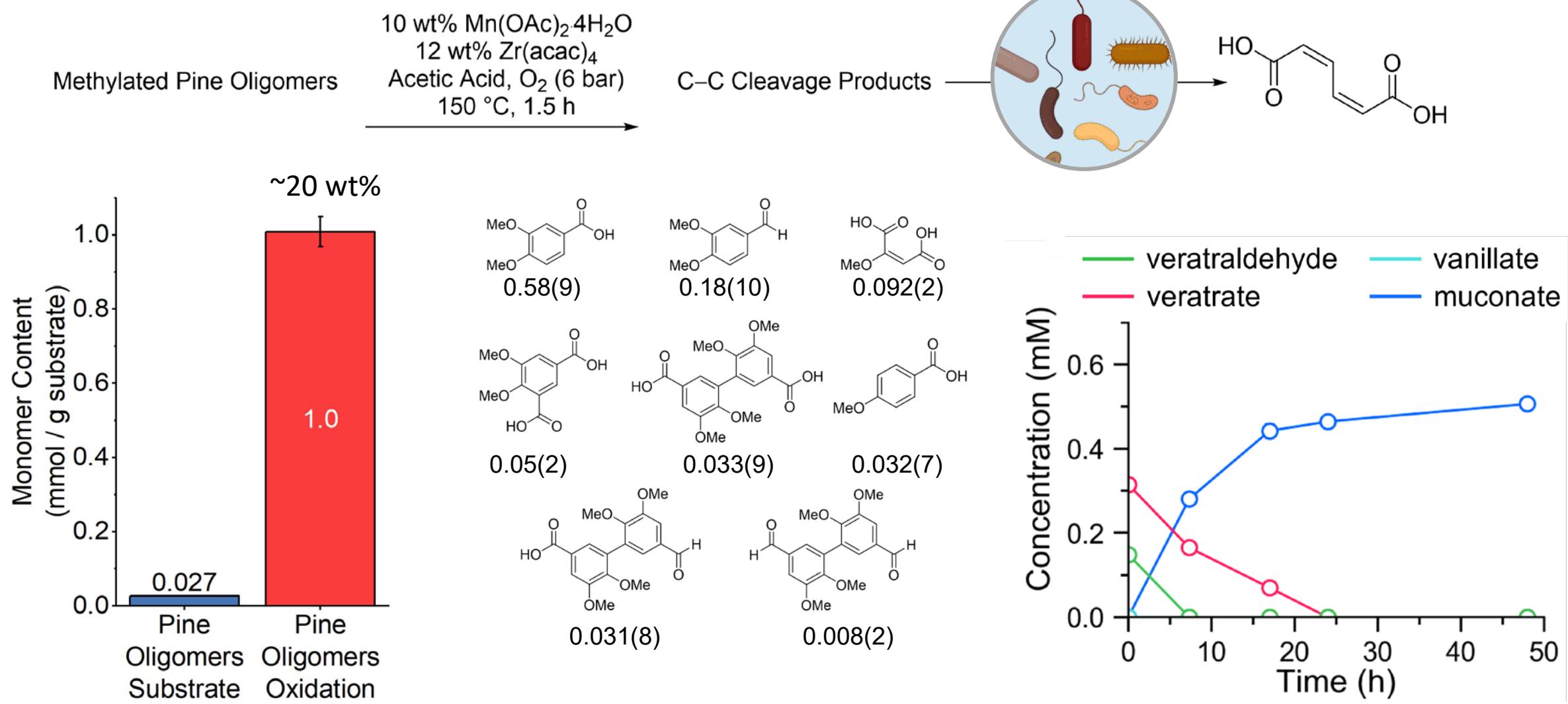
Optimization of Mn-Autoxidation of Pine Oligomers in Batch



Optimized Mn-Autoxidation of Pine Oligomers in Batch



Optimized Mn-Autoxidation of Pine Oligomers in Batch



NREL

Gregg T. Beckham

Alissa Bleem

Nina X. Gu

David G. Brandner

Jeremy R. Bussard

Kevin P. Sullivan

Mikhail O. Konev

Jacob K. Kenny

Stefan J. Haugen

Kelsey J. Ramirez

Morgan A. Ingraham

Caroline R. Amendola

SLAC

Arun S. Asundi

Ritimukta Sarangi

UW-Madison

Prof. Shannon S. Stahl

Thank You

www.nrel.gov

NREL/PR-2800-87188

This work was authored by the National Renewable Energy Laboratory, operated by Alliance for Sustainable Energy, LLC, for the U.S. Department of Energy (DOE) under Contract No. DE-AC36-08GO28308. Funding provided by the U.S. Department of Energy Office of Energy Efficiency and Renewable Energy Bioenergy Technologies Office. The views expressed in the article do not necessarily represent the views of the DOE or the U.S. Government. The U.S. Government retains and the publisher, by accepting the article for publication, acknowledges that the U.S. Government retains a nonexclusive, paid-up, irrevocable, worldwide license to publish or reproduce the published form of this work, or allow others to do so, for U.S. Government purposes.



On the Academic Job Market this Year...

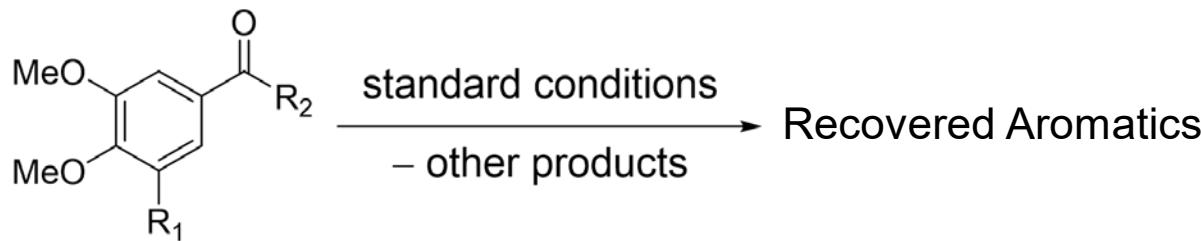
On the job market...



Chad T. Palumbo, Ph.D.

email: palumbochad@gmail.com

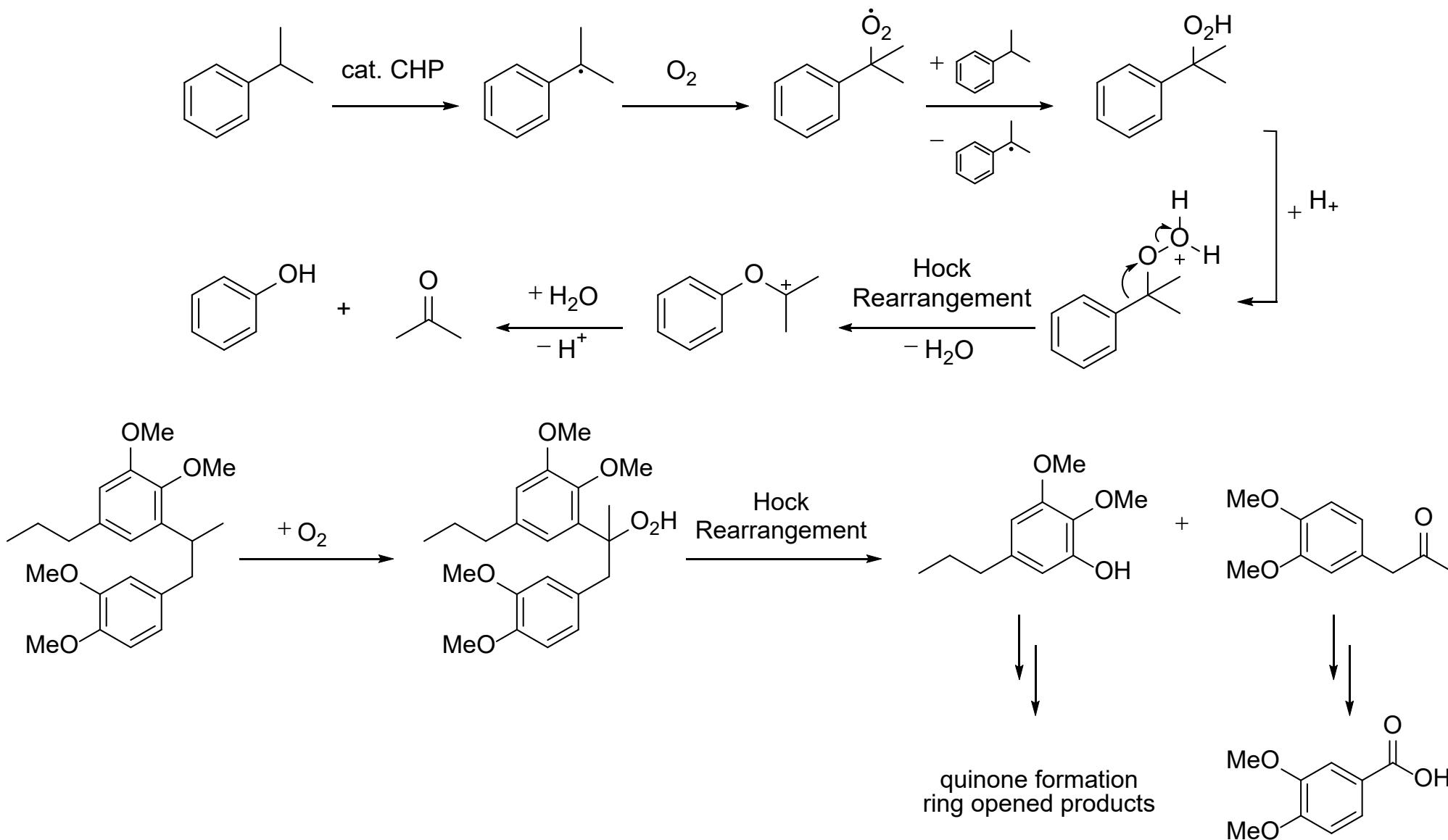
Studies of Stability of Carboxylic Acids in Autoxidation Conditions



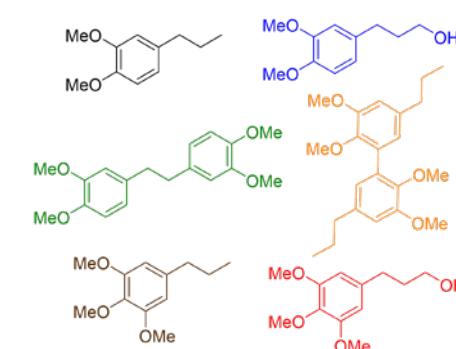
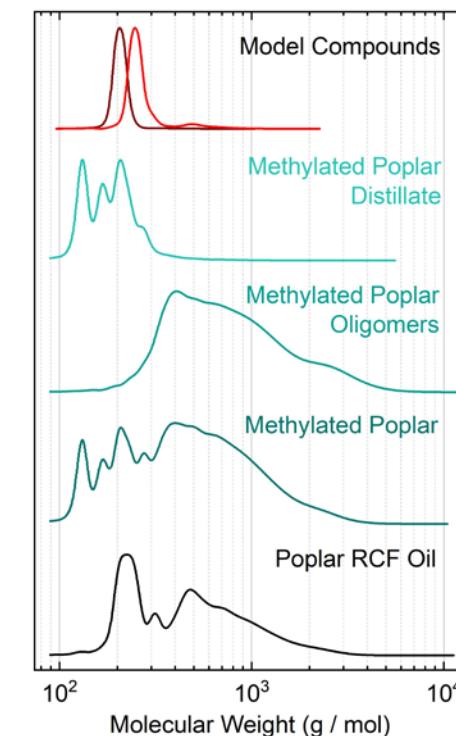
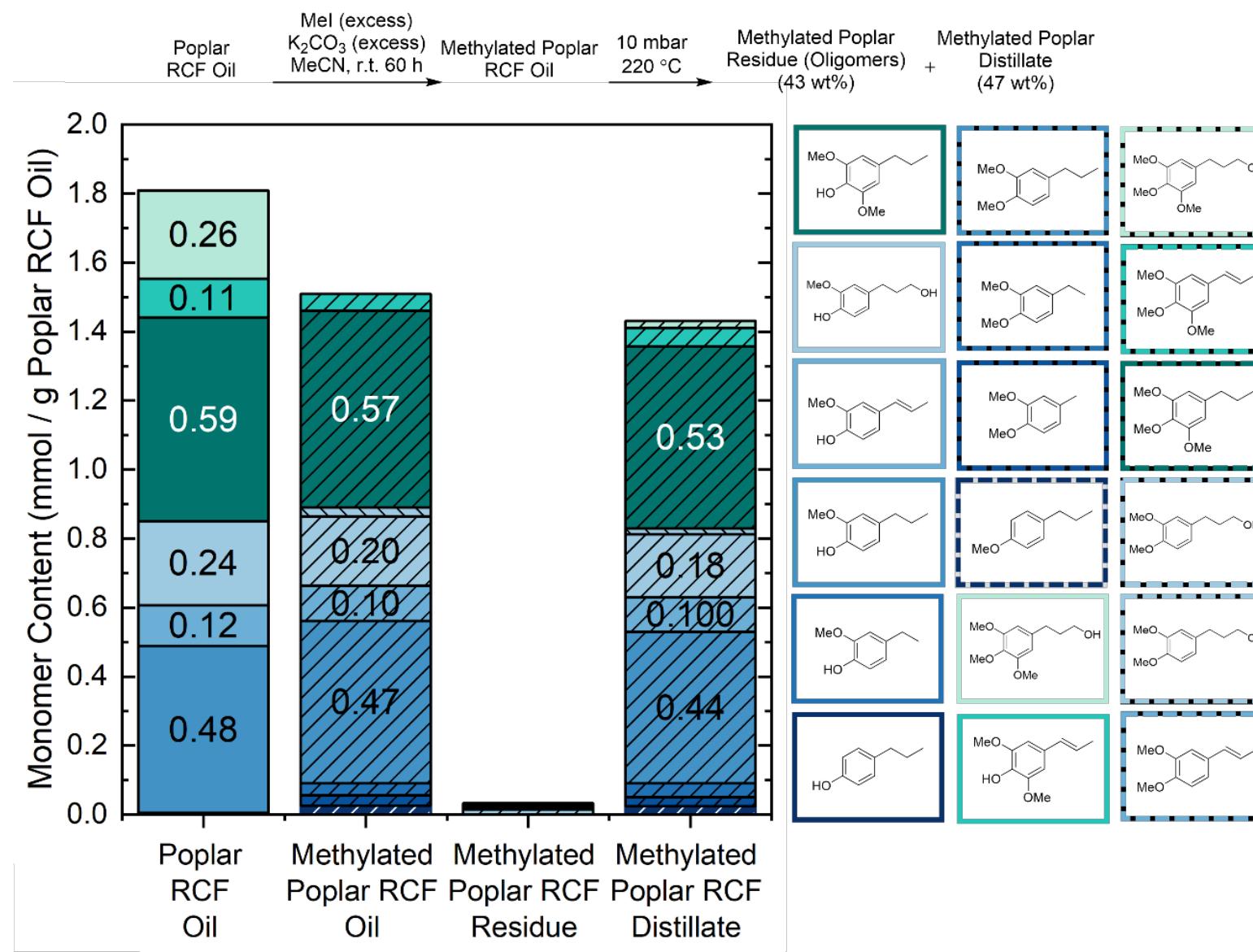
standard conditions =
8 mol% $\text{Mn}(\text{OAc})_2 \bullet 4\text{H}_2\text{O}$
6 mol% $\text{Zr}(\text{acac})_4$
6 bar O_2 , 150 °C
15 mL AcOH, 1.5 h

R_1	R_2	Aromatic Recovery (%)
H	H	38(4)%
H	OH	62(7)%
OMe	H	43%
OMe	OH	51(12)%

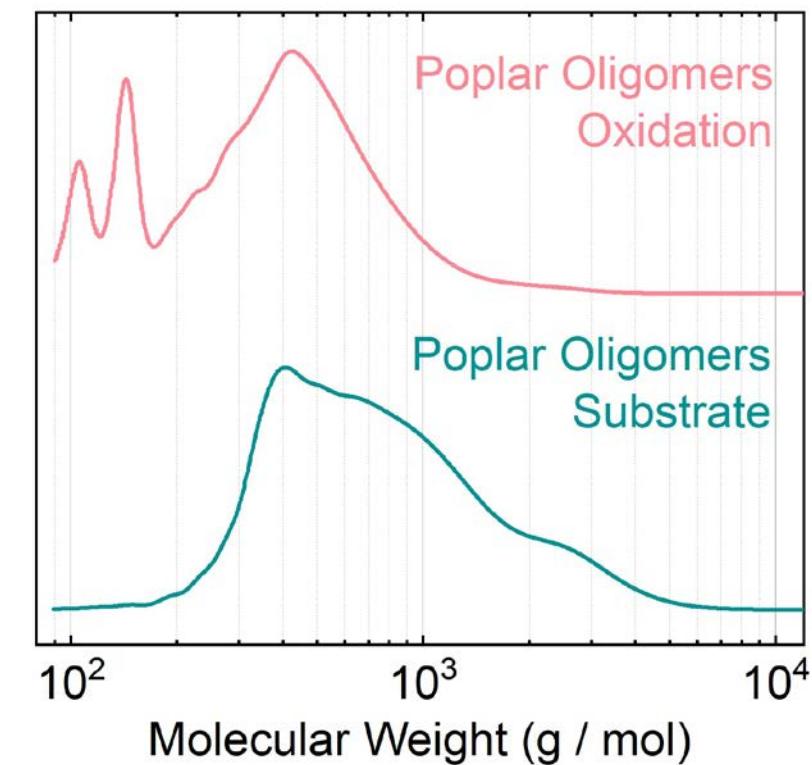
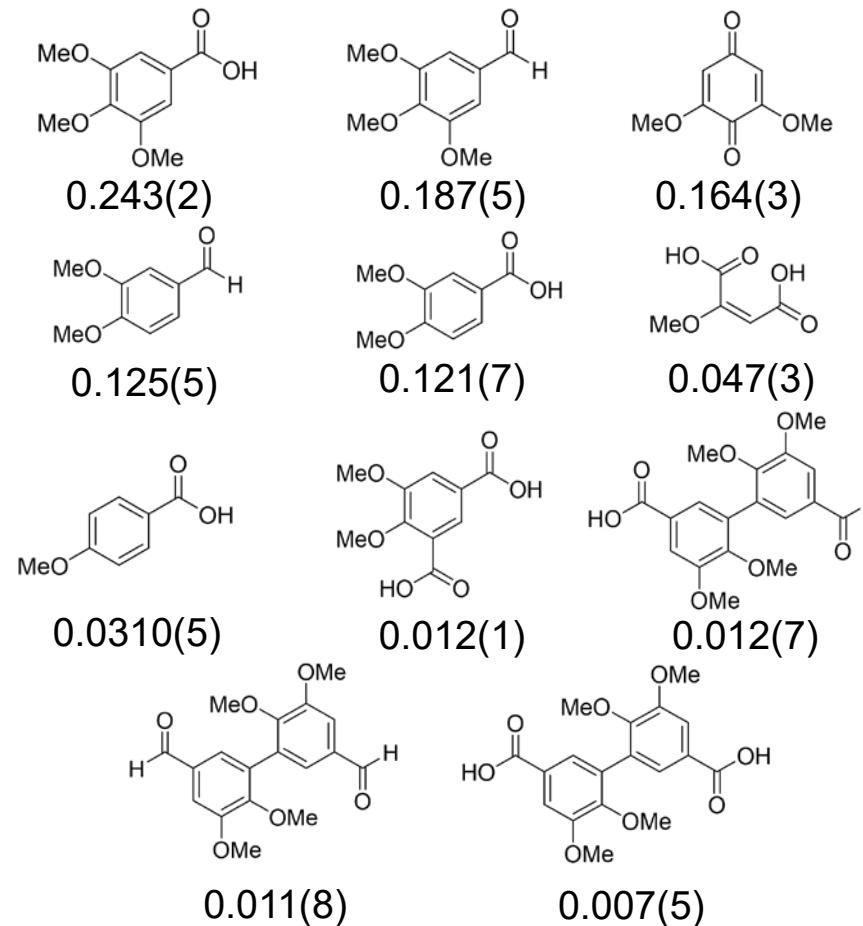
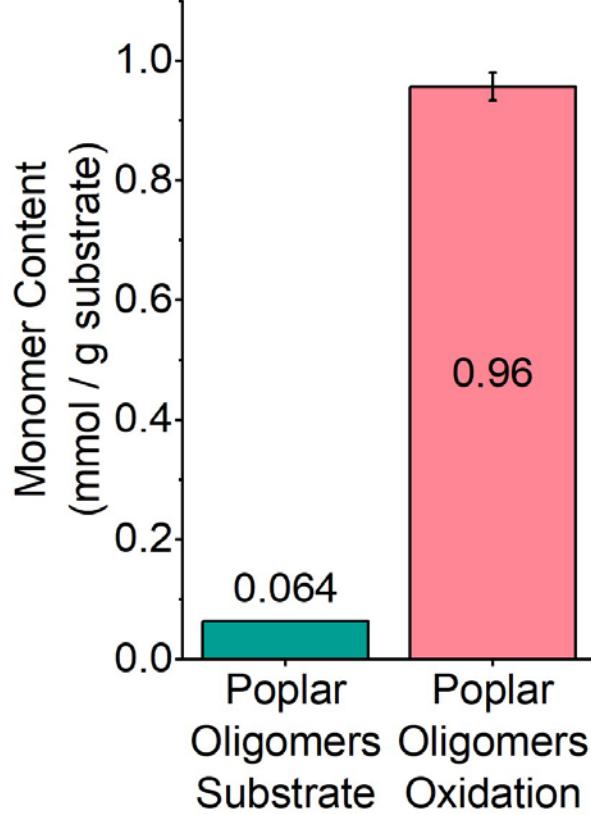
The Cumene Process and Hock Rearrangement



Preparation and Autoxidation of Methylated Poplar Oligomers



Preparation and Autoxidation of Methylated Poplar Oligomers



Bioconversion Pathway

