

High-Fidelity and High-Performance Computational Simulations for Rapid Design Optimization of Sulfur Thermal Energy Storage

Program: HPC4EI (High Performance Computing for Energy Innovation)

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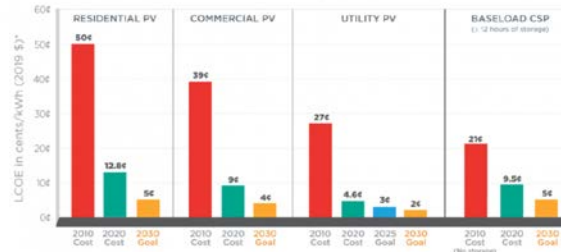
Sulfur based energy storage



Current methods of storage

- Two-tank solar salt storage concept for the IPH temperature range of 100-300 °C is prohibitively expensive
- Latent-based phase change materials (PCMs) and sensible-based solid-state thermal storage media (concrete, rocks) suffers from **high storage cost, poor thermal responsiveness, and/or thermal cyclic stability concerns.**

Solar Energy Technologies Office Progress and Goals
Photovoltaics (PV) and Concentrating Solar-Thermal Power (CSP)



*Levelized cost of energy (LCOE) PV progress and targets are calculated based on average U.S. climate and without the Investment Tax Credit or state/local incentives.

Table IV. Benchmark parameters for a 100 MW CSP system with 14 hours thermal storage.³⁶

Parameter	2018 Benchmark ^{37,38}	2030 Low-Cost	2030 Balanced	2030 High-Performance
Net power-cycle efficiency	37%	40%	50%	55%
Rated thermal power	730 MW _{thermal}	675 MW _{thermal}	540 MW _{thermal}	481 MW _{thermal}
Power block cost	\$1330/kW _{ac-gross}	\$700/kW _{ac-gross}	\$900/kW _{ac-gross}	\$900/kW _{ac-gross}
Solar field cost	\$140/m ²	\$50/m ²	\$50/m ²	\$70/m ²
Site preparation cost	\$16/m ²	\$10/m ²	\$10/m ²	\$10/m ²
Tower and receiver cost	\$137/kW _{thermal}	\$100/kW _{thermal}	\$120/kW _{thermal}	\$120/kW _{thermal}
Thermal storage cost	\$22/kWh _{thermal}	\$10/kWh _{thermal}	\$15/kWh _{thermal}	\$15/kWh _{thermal}
Levelized O&M cost ³⁹	\$0/kWh _{thermal-yr}	\$0/kWh _{thermal-yr}	\$7/kWh _{thermal-yr}	\$7/kWh _{thermal-yr}
Levelized capacity factor	68.9%	69.2%	70.7%	71.0%
LCOE (2019 US\$) ⁴⁰	5.8¢/kWh	5.0¢/kWh	5.0¢/kWh	5.0¢/kWh

Sulfur based storage*

- Sulfur is a cheap commodity at \$80/ton compared to \$1100 - 1300/ton for conventional salts and costs around 2-3 \$/kWh
- High energy storage density
- Sulfur-based TES have 3-14 times higher charge-discharge rates than PCM-TES

Less than DOE target of \$15/kW_{th} for thermal storage⁺



Better performance

Parameter	2018 Benchmark ^{37,38}	2030 Low-Cost	2030 Balanced	2030 High-Performance
Thermal storage cost	\$22/kWh _{thermal}	\$10/kWh _{thermal}	\$15/kWh _{thermal}	\$15/kWh _{thermal}

* Nithyanandam, Karthik, et al. No. DE-FE0032007-Element16-Final Report. Element 16 Technologies, Inc., Glendale, CA (United States), 2022.
+ Murphy, Caitlin, et al. National Renewable Energy Lab.(NREL), Golden, CO (United States), 2019.

Sulfur TES Study design



Goals:

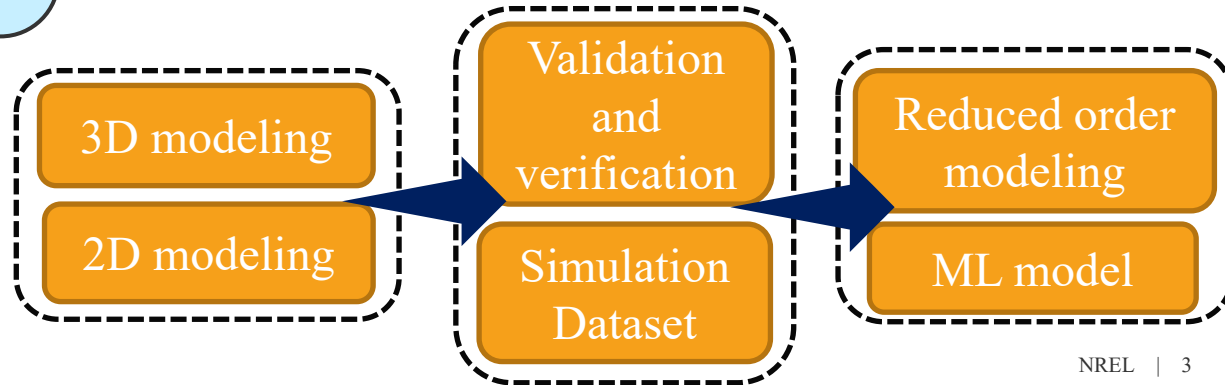
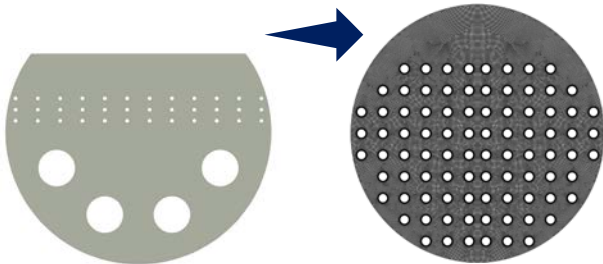
- Validate Numerical model
- Design either correlation for HTC/Temperature behavior of sulfur with time (charge/discharge)
- Develop tool to predict design of TES for a given thermal output of the system (product aimed at IPH application)



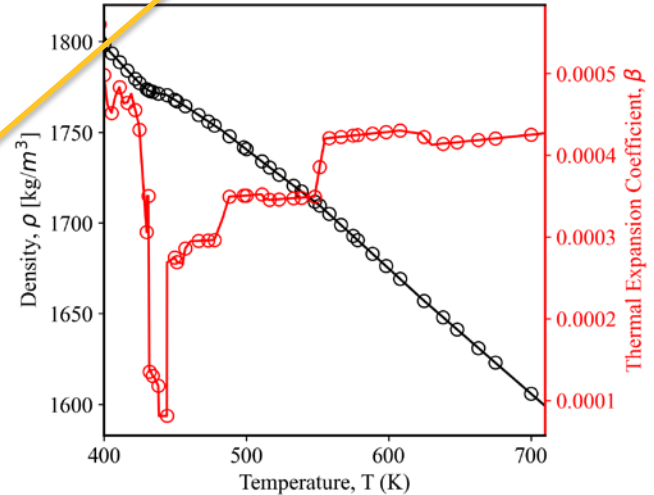
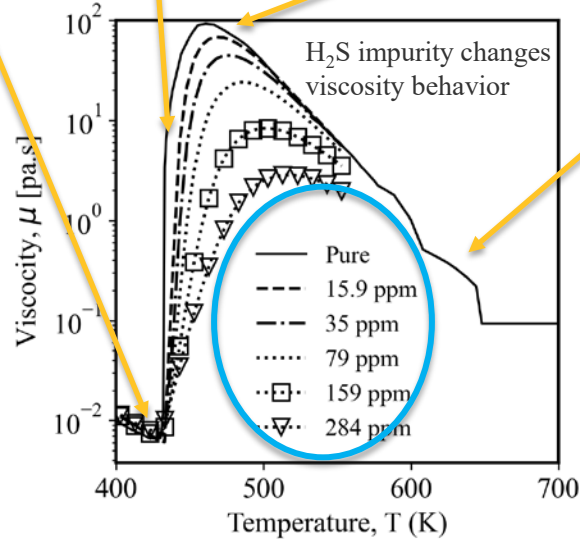
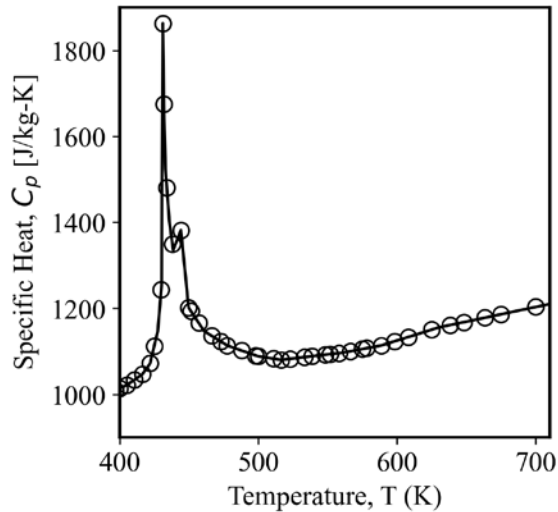
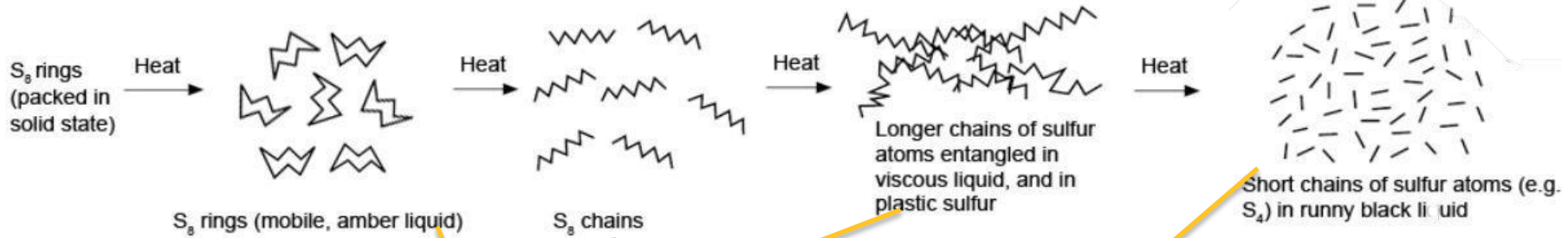
Element 16's 350KWh pilot sulfur TES prototype

Pilot prototype

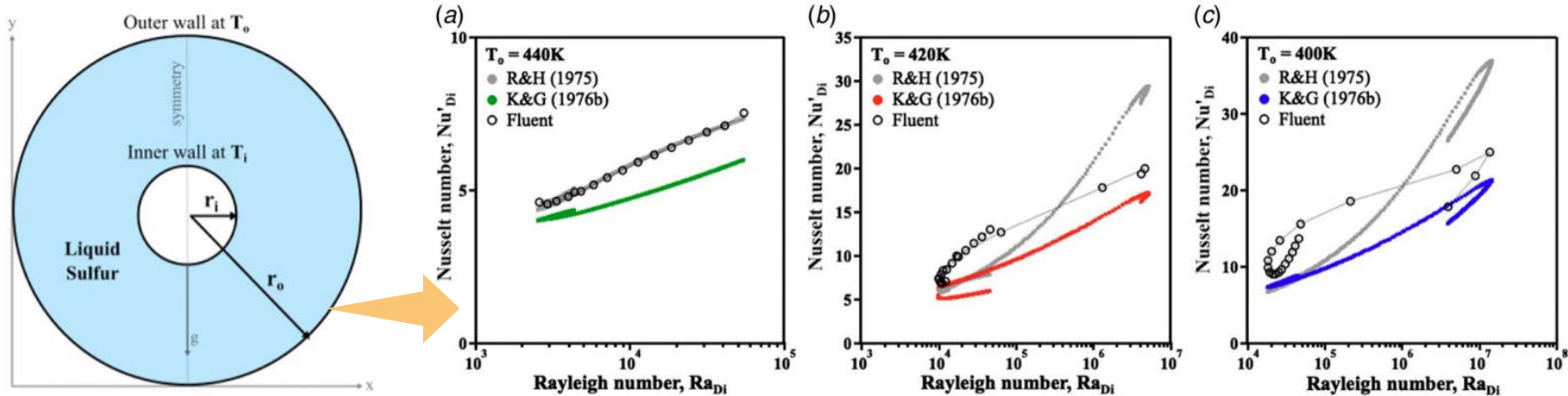
Product



Sulfur properties



Why not empirical correlations?

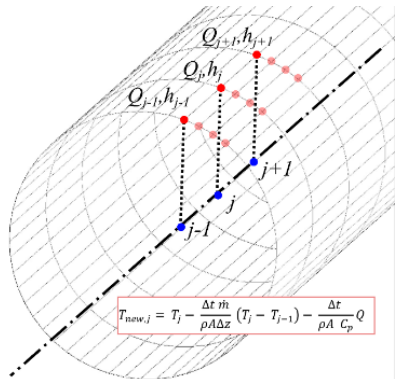
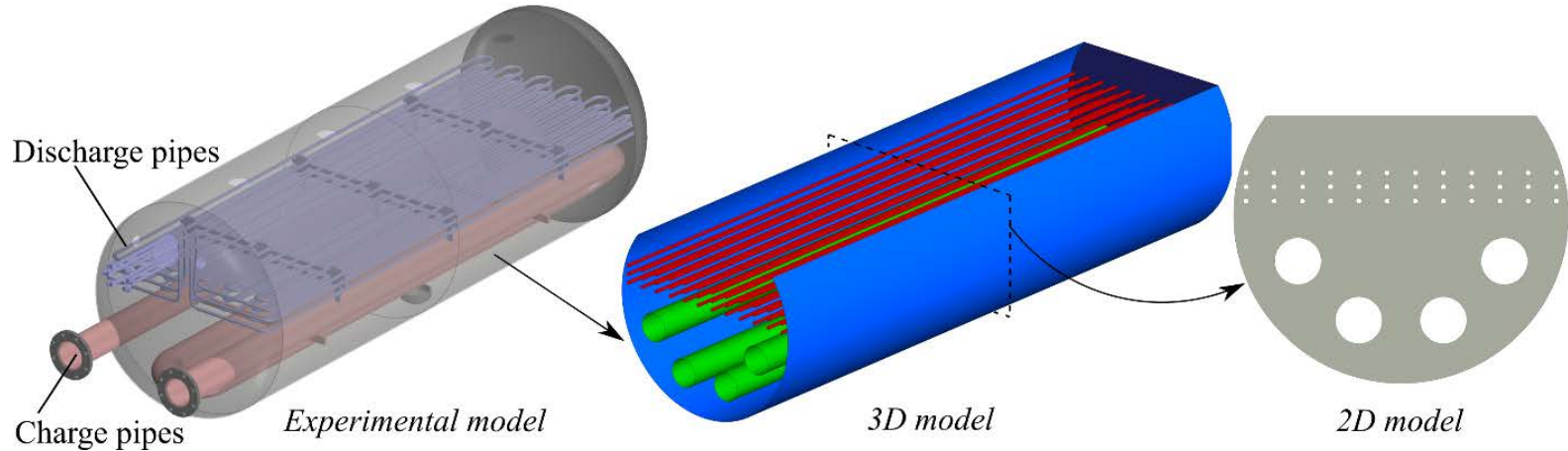


Correlation failure for commonly known two-cylinder Nu-Ra correlations because of,

- Heat transfer ability of sulfur begins to show unconventional fluctuations with respect to temperature gradient as sulfur chains break apart.
- Rapid shifts in sulfur viscosity with increasing temperature
- Heat transfer physics and convective flow behaviors of the fluid are significantly altered with change in viscosity
- Resulting in an unpredictable and highly nonuniform distribution of fluid properties throughout the TES.



Modeling approach



$$T_{new,j} = T_j - \frac{\Delta t \dot{m}}{\rho A \Delta z} (T_j - T_{j-1}) - \frac{\Delta t}{\rho A C_p Q}$$

HTF temperature profile predicted by UDF

Heat transfer rate at the wall of tube j

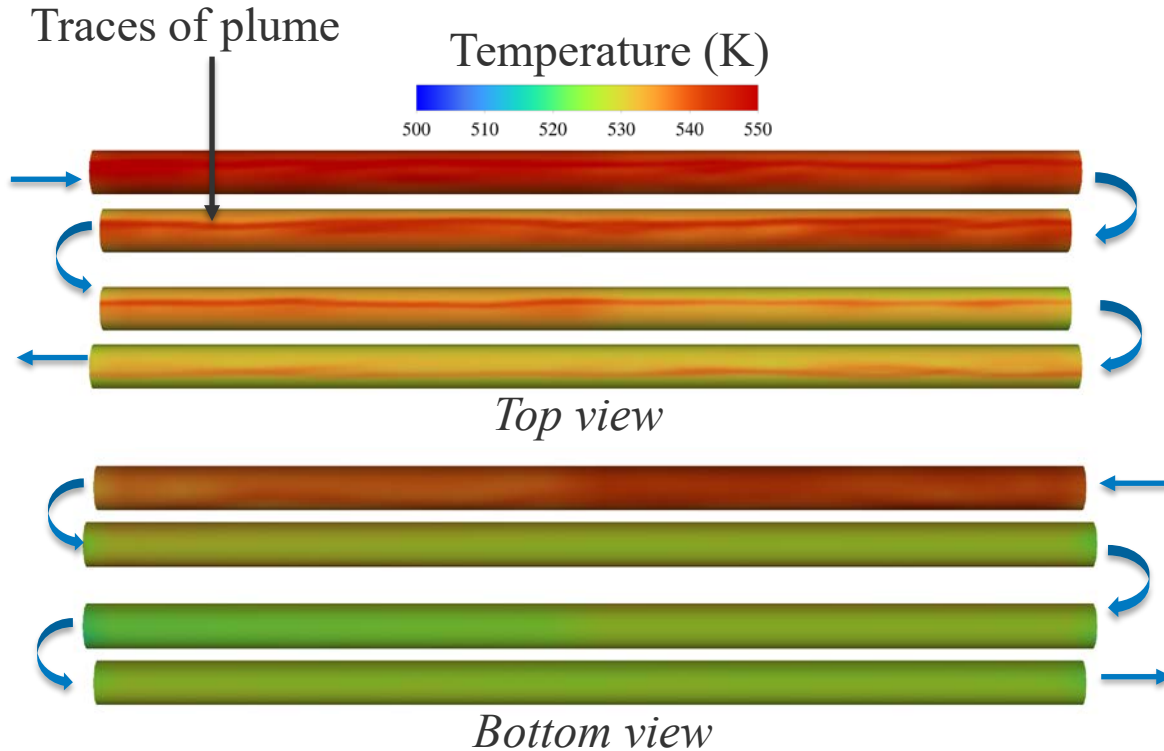
$$\rho C_p A_c \frac{\partial T_f(z, t)}{\partial t} + \dot{m} C_p \frac{\partial T_f(z, t)}{\partial z} = -Q_{tube,j}(z, t)$$

Explicit finite difference methods

Sum of heat transfer rates for all tube wall mesh elements in the CFD model assigned to reduced-order model axial element i

$$T_f^{i,t+1} = T_f^{i,t} - \frac{\dot{m} \Delta t}{\rho A_c \Delta z} (T_f^{i,t} - T_f^{i-1,t}) - \frac{Q_{tube,j}^{i,t} \Delta t}{\rho C_p A_c}$$

Temperature profile

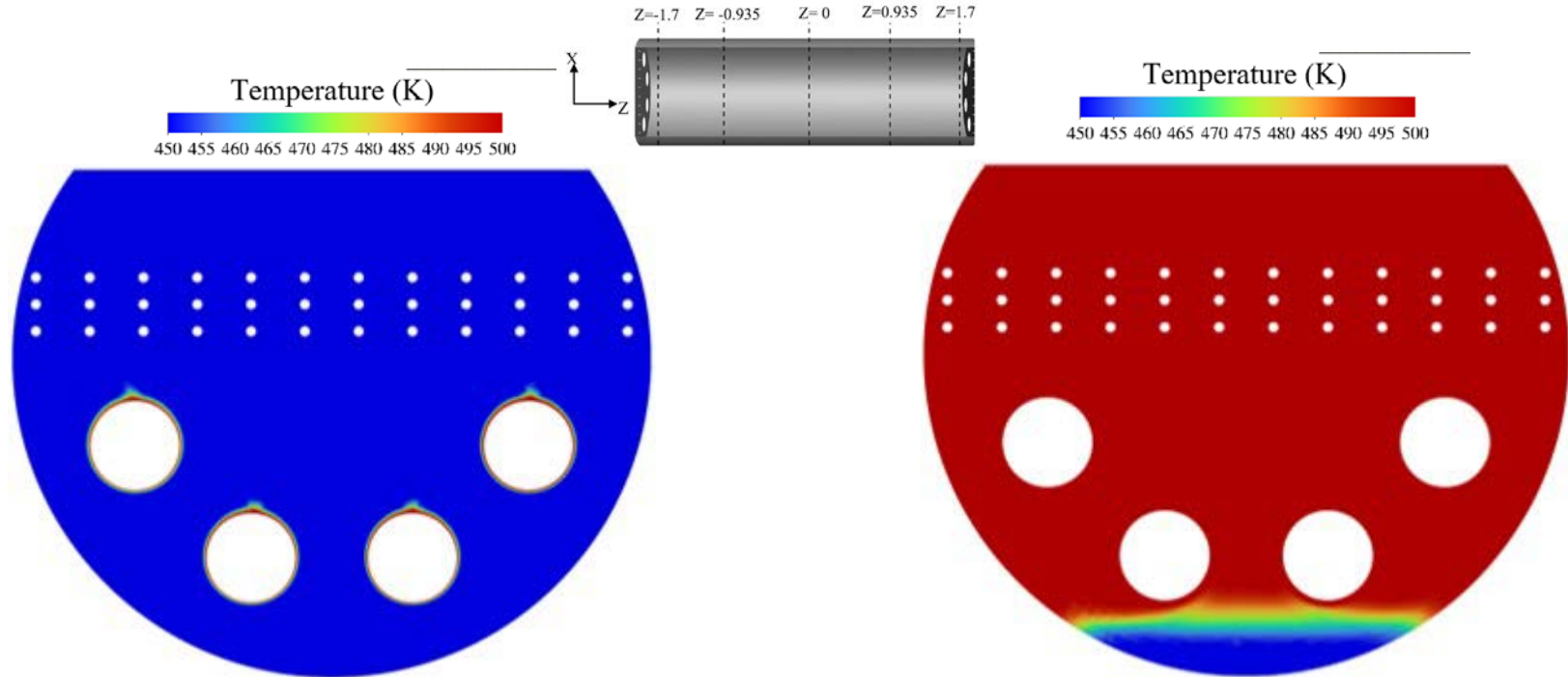


$$t = 11.11\text{Hr}$$

Temperature gradient across charge pipes based on the convective boundary condition.

- Air at higher temperature enters charge pipes, navigates through four passes, and exits with lower temperature by charging sulfur inside domain to higher temperature.
- Top view of the charge pipes demonstrates traces of high temperature location across the length, elucidating convection of sulfur and location of plume detachment from charge pipe.
- Evident temperature difference in top and bottom view of charge pipes facilitates natural convection occurring through radial temperature gradient.

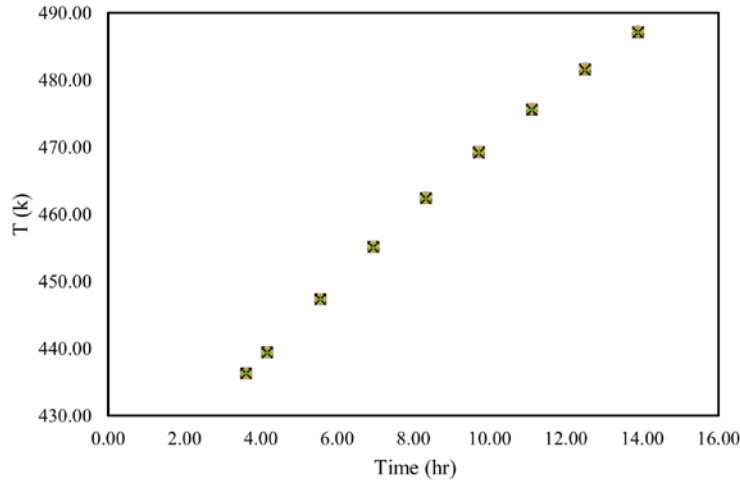
3D simulations - Charge and Discharge



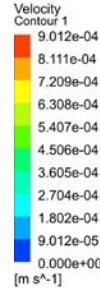
$t = 3.6$ to 13.8 hr at
Midplane ($z=0$) of tank

$t = 20.8$ to 26.8 hr at
Midplane ($z=0$) of tank

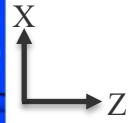
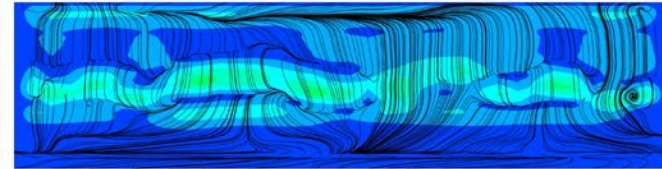
3D simulations- Axial and cross flow



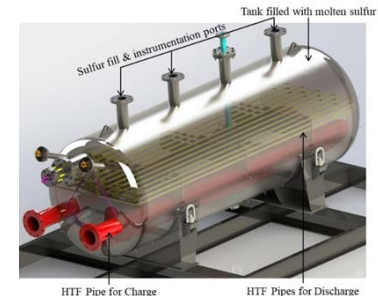
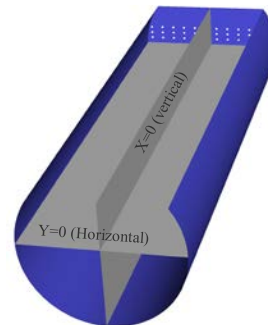
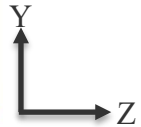
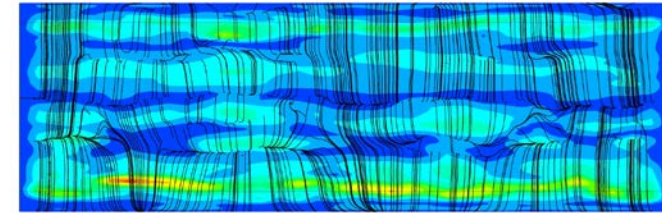
- Total (Volume averaged)
- $z = -1.7$ (Surface averaged)
- × $z = +0.935$ (Surface averaged)
- △ $z = -0.935$ (Surface averaged)
- ◇ $z = 0$ (Surface averaged)
- + $z = +1.7$ (Surface averaged)



Y=0 (Horizontal)



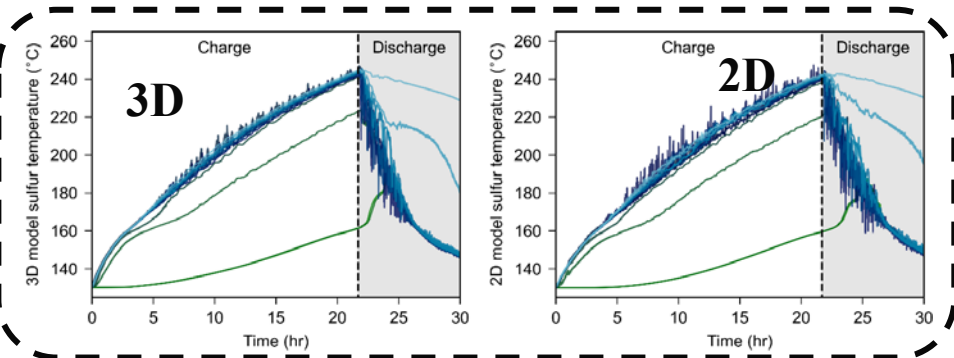
X=0 (vertical)



- 2D cross section from the prototype tank can give an accurate representation of the bulk average temperature and viscosity in tank
- The two-dimensionality of heat transfer mechanism within the TES can be useful in ML modeling and optimization of system

Summary of Modeling

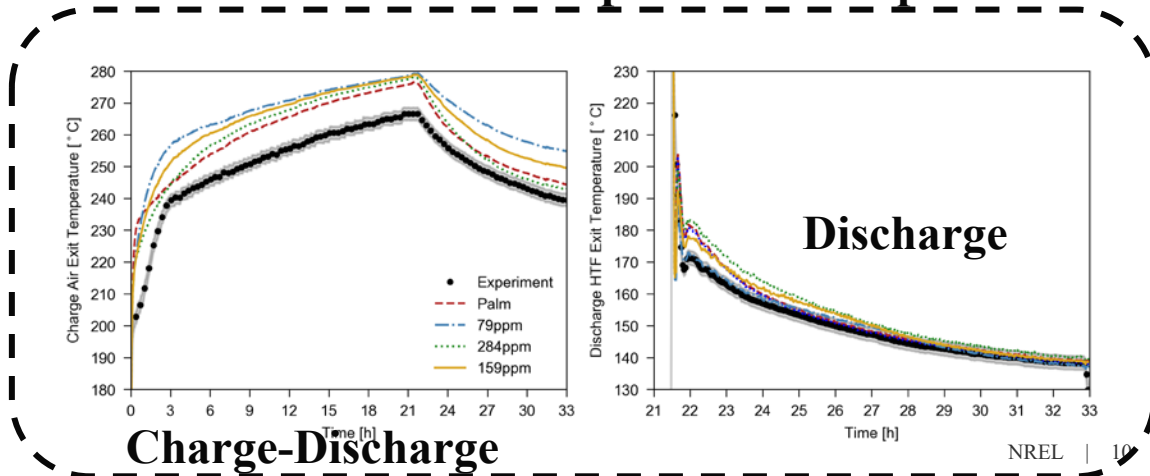
3D vs 2D



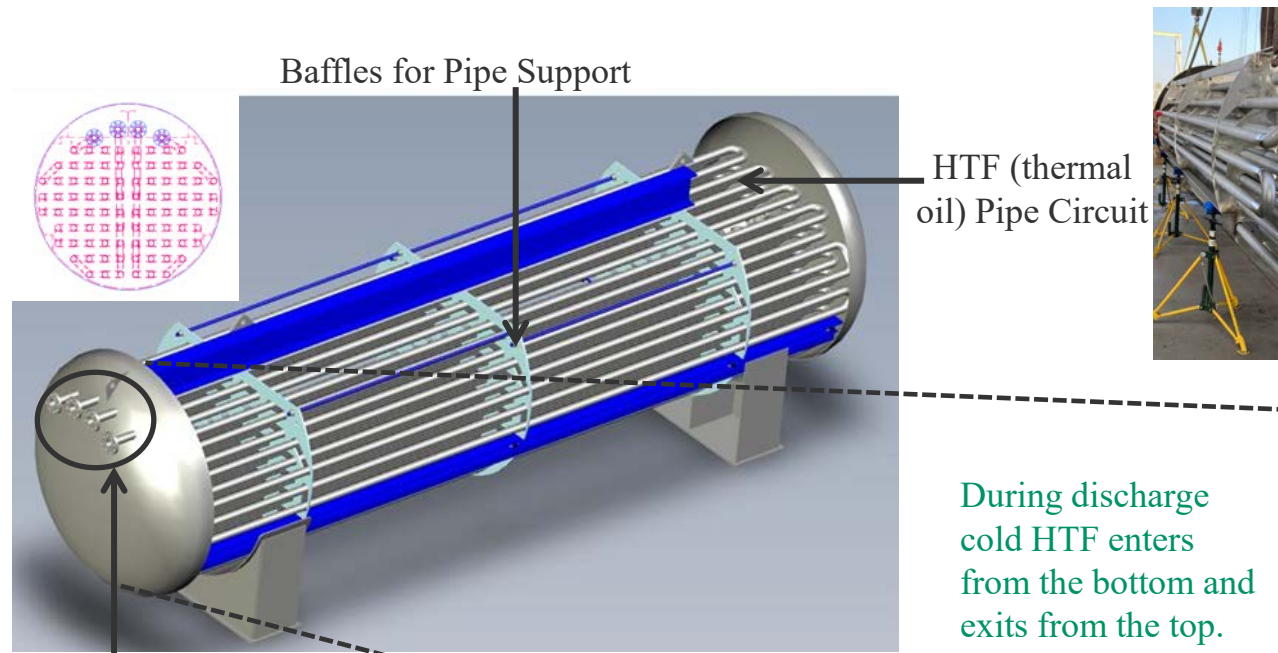
- Computations capture physical TES behavior
- Outlet temperature measurement had heat loss

- Absence of three dimensionality in sulfur TES
- 2D simulation can be used for ROM and optimization.

Computation vs Exp



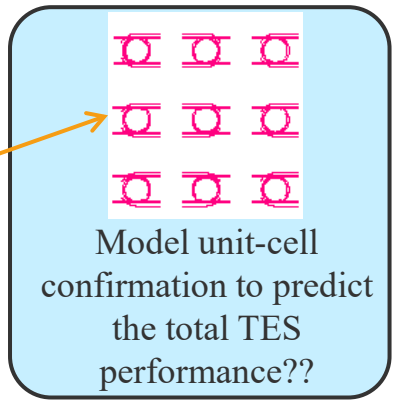
Sulfur TES Design for solar thermal integration



Baffles for Pipe Support

HTF (thermal oil) Pipe Circuit

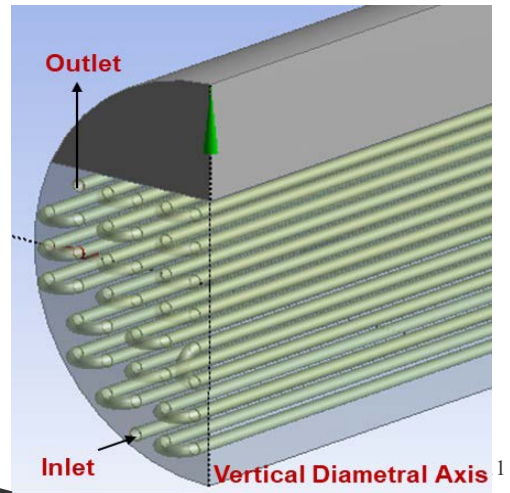
Interface to HTF Pipe Circuits



Model unit-cell confirmation to predict the total TES performance??

The diagram shows a 3x3 grid of unit cells, each containing a pipe with a baffle. An arrow points from the grid to the photograph of the tank.

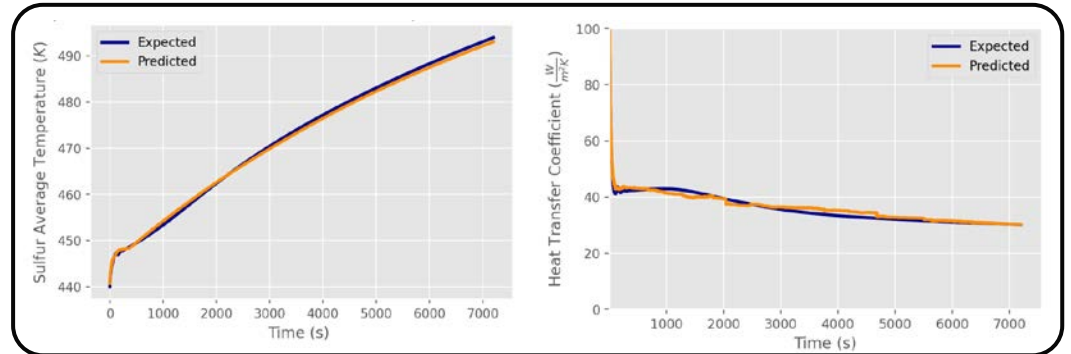
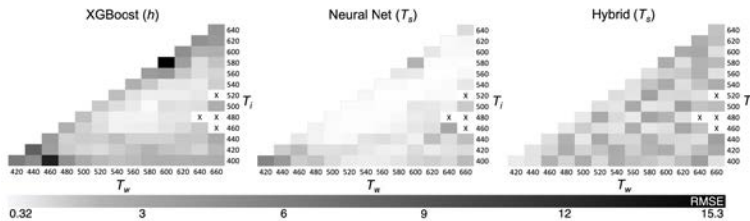
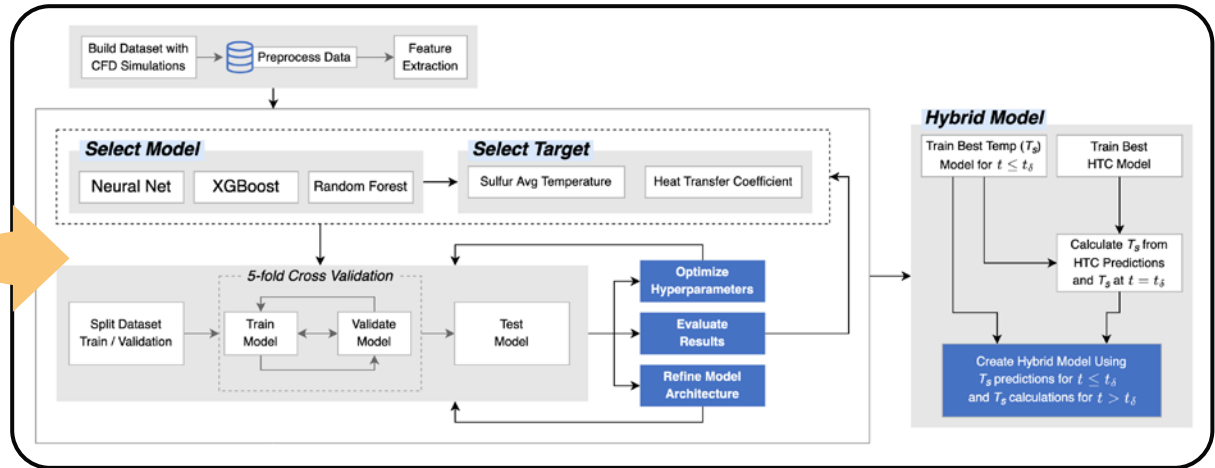
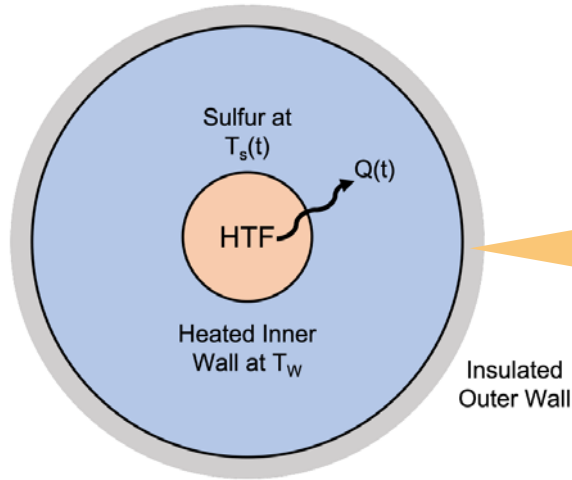
During discharge cold HTF enters from the bottom and exits from the top. During charge, the flow direction is reversed



Schematic depicted here for a 1.5 MWh system that is being built



Surrogate Model



Acknowledgments



Zhiwen Ma
(NREL)



Michael Martin
(NREL)



Janna Martinek
(NREL)



Dmitry Duplyakin
(NREL)



Karthik
Nithyanandam (E16)



Mohammad
Rahimi (NREL)



Madeleine
Oliver



Kevin
Menear (NREL)

Thank you! Questions?

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NREL/PR-5700-90576

This work was authored by the National Renewable Energy Laboratory, operated by Alliance for Sustainable Energy, LLC, for the U.S. Department of Energy (DOE) under Contract No. DE-AC36-08GO28308. Funding was provided by the Advanced Manufacturing Office's HPC4EI (High Performance Computing for Energy Innovation) program through the project "Optimization of Sulfur Thermal Energy Storage." The research was performed using computational resources sponsored by the Department of Energy's Office of Energy Efficiency and Renewable Energy and located at the National Renewable Energy Laboratory. The views expressed in the article do not necessarily represent the views of the DOE or the U.S. Government. The U.S. Government retains and the publisher, by accepting the article for publication, acknowledges that the U.S. Government retains a nonexclusive, paid-up, irrevocable, worldwide license to publish or reproduce the published form of this work, or allow others to do so, for U.S. Government purposes.